

Reciprocating Compressor

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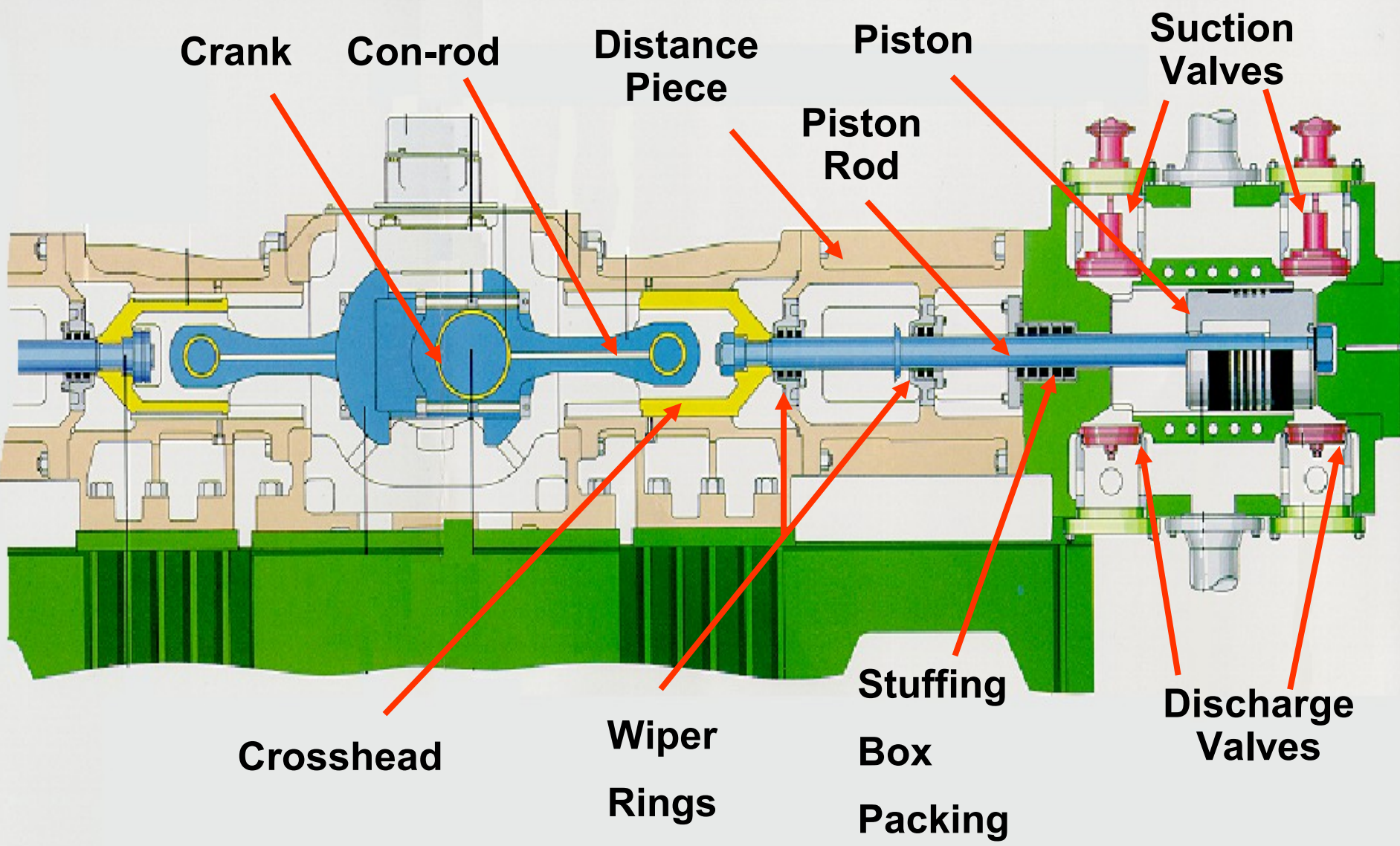
Efficiency and Energy Conservation Laboratory
Diponegoro University

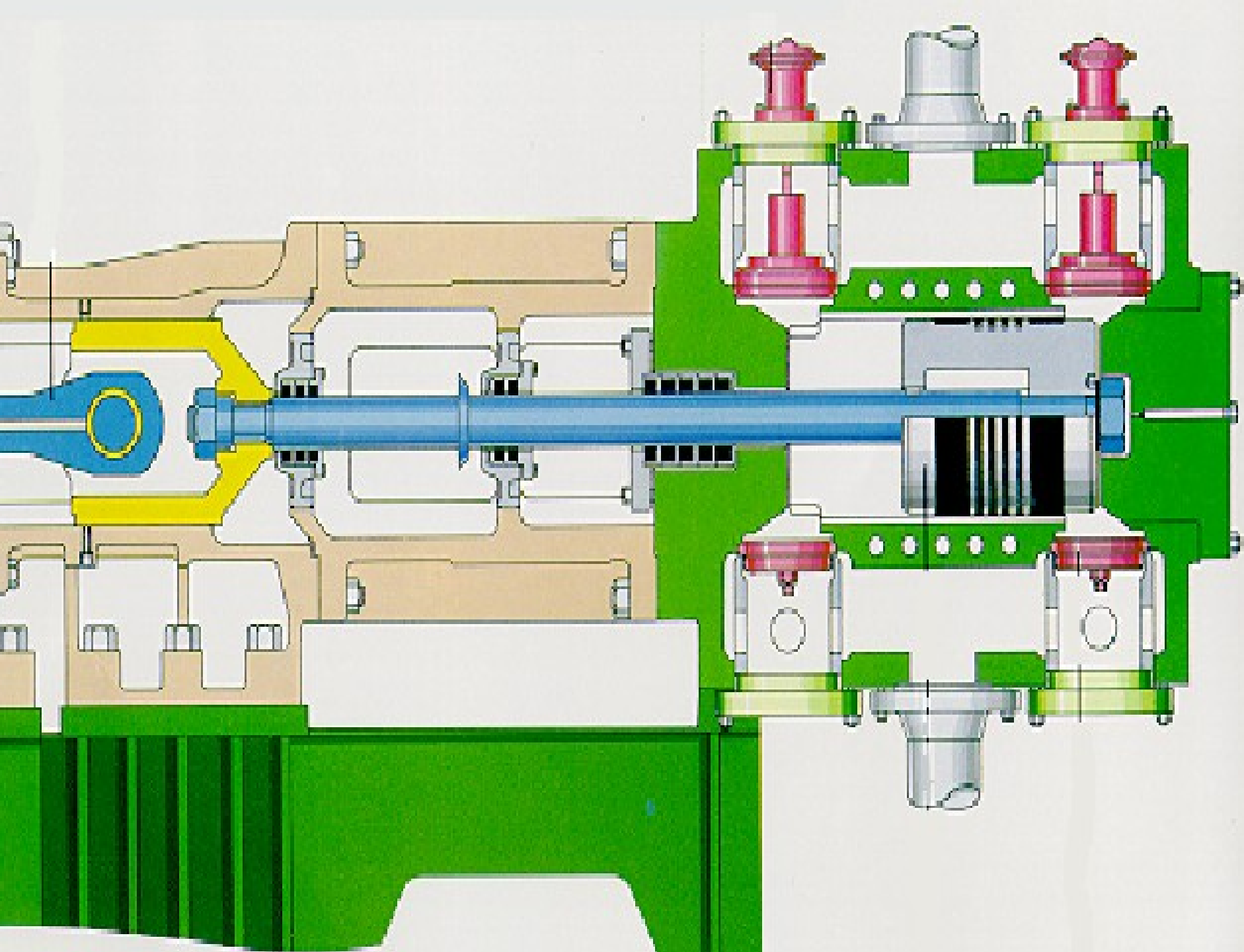


RECIPROCATING COMPRESSORS

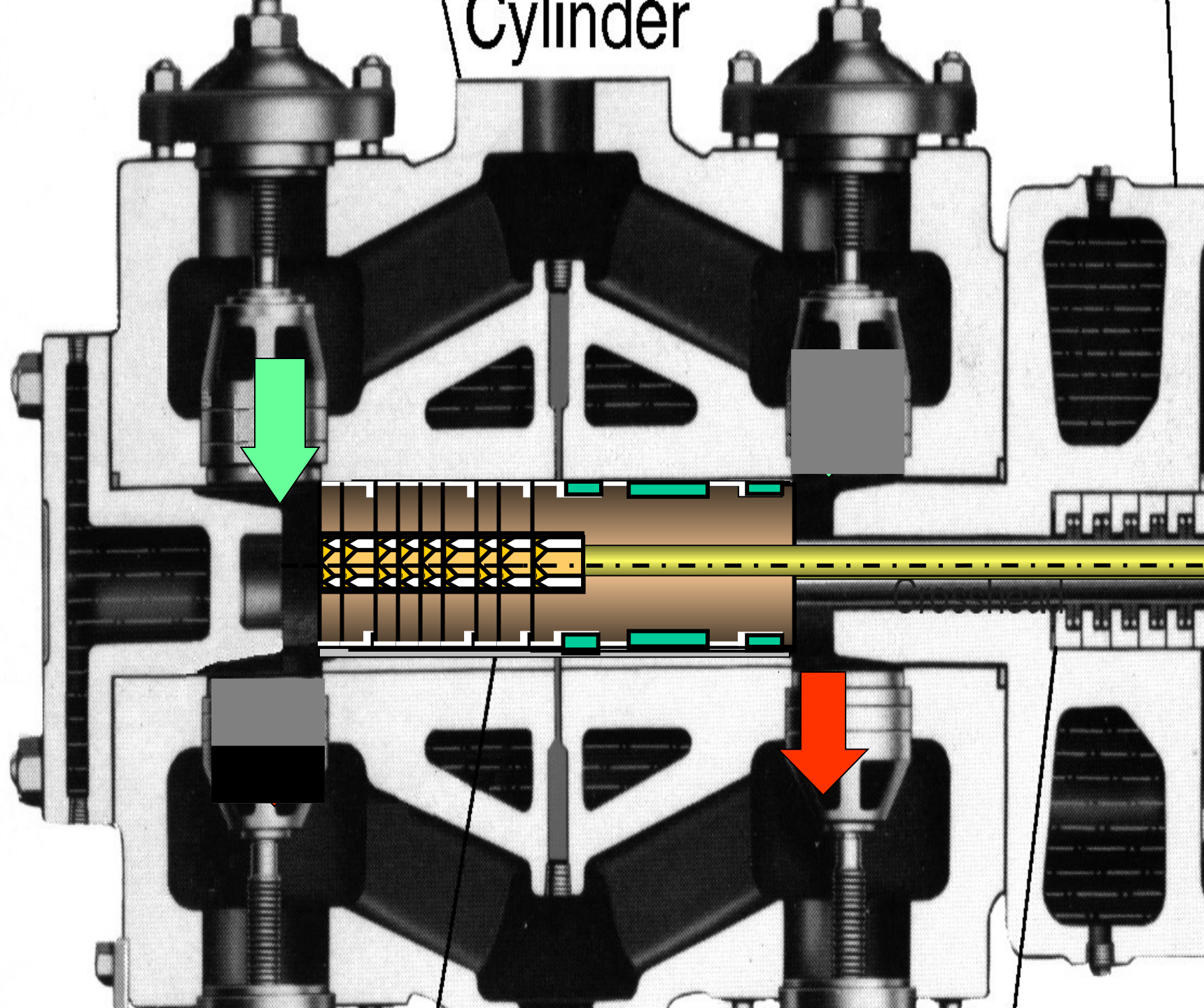
Compressors

	Reciprocating	Centrifugal	Axial
Pressure P	V. HIGH	HIGH	LOW
Flow Rate Q	LOW	HIGH	V. HIGH
S .R .V	YES	NO	NO
Efficiency	LOW	HIGH	V. HIGH
Maint. cost	V. HIGH	LOW	LOW
Pulsation	YES	NO	NO
Surging	NO	YES	YES





Cylinder



Cross-section

POWER END

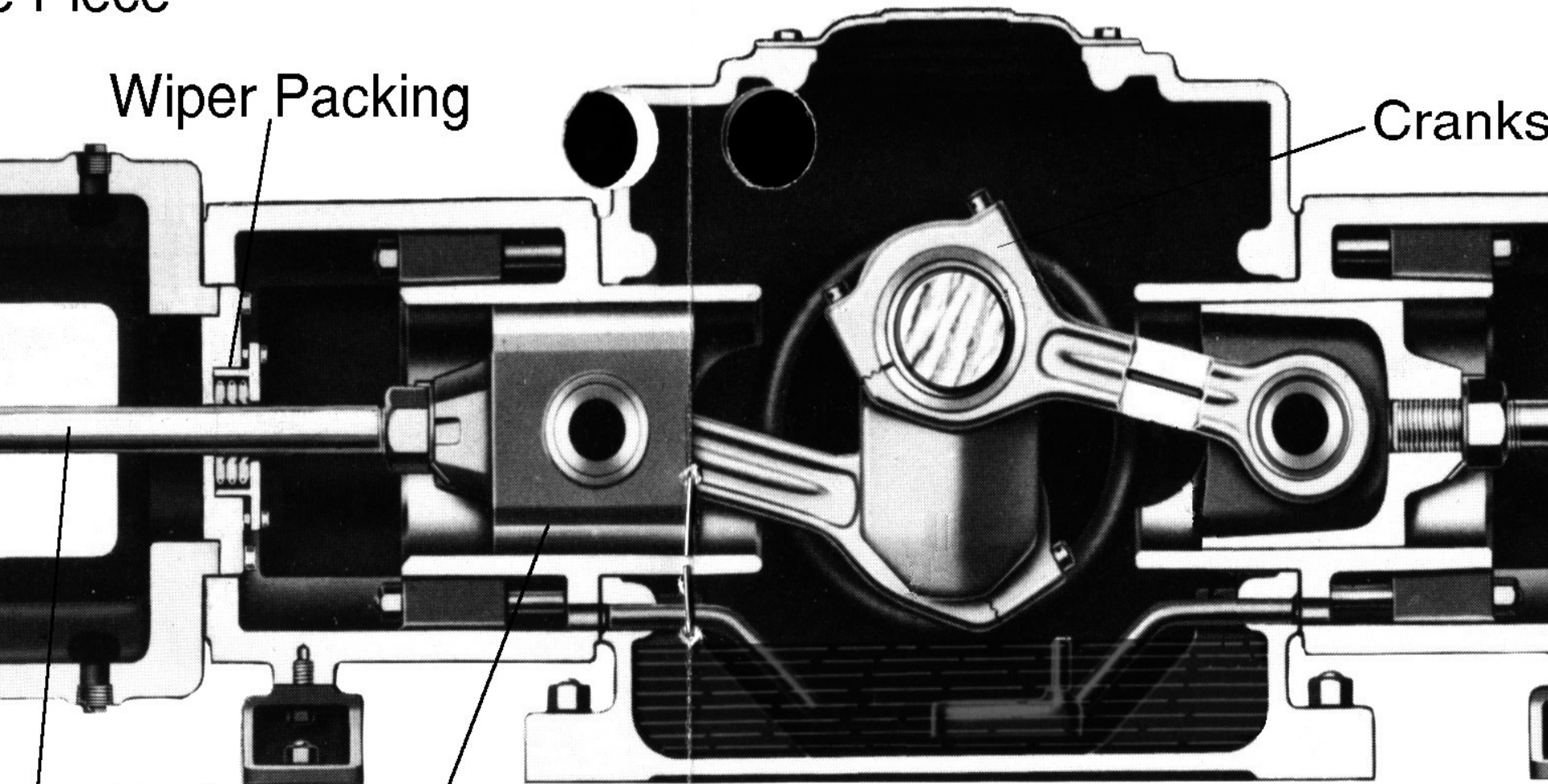
e Piece

Wiper Packing

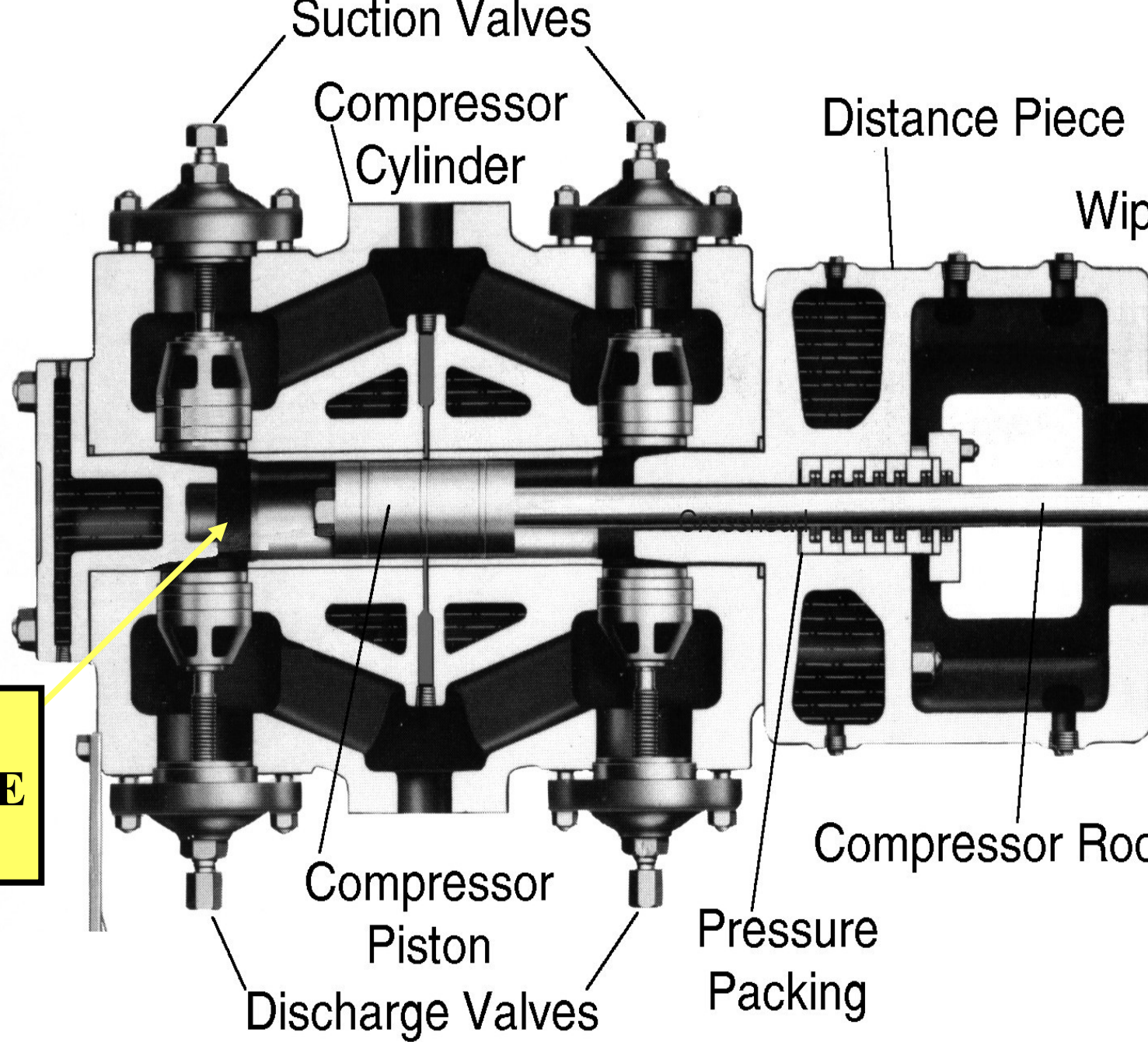
Cranks

ssor Rod

Crosshead

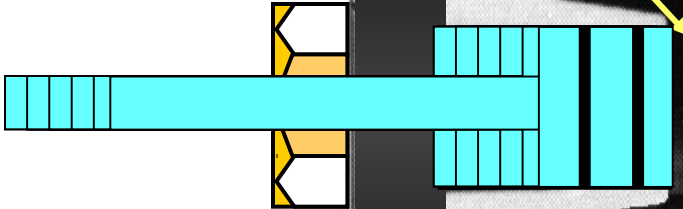


**GAS
END**



**FIXED
CLEARANCE
VOLUME**

**VARIABLE
CLEARANCE
VOLUME**



Cylinder

Cross-section

Com

RECIPROCATING COMPRESSORS: FLOW RATE REGULATION

- **VARIABLE CLEARANCE**

- **SUCTION VALVE
UNLOADERS**

- **VARIABLE SPEED**

- **BYPASS**

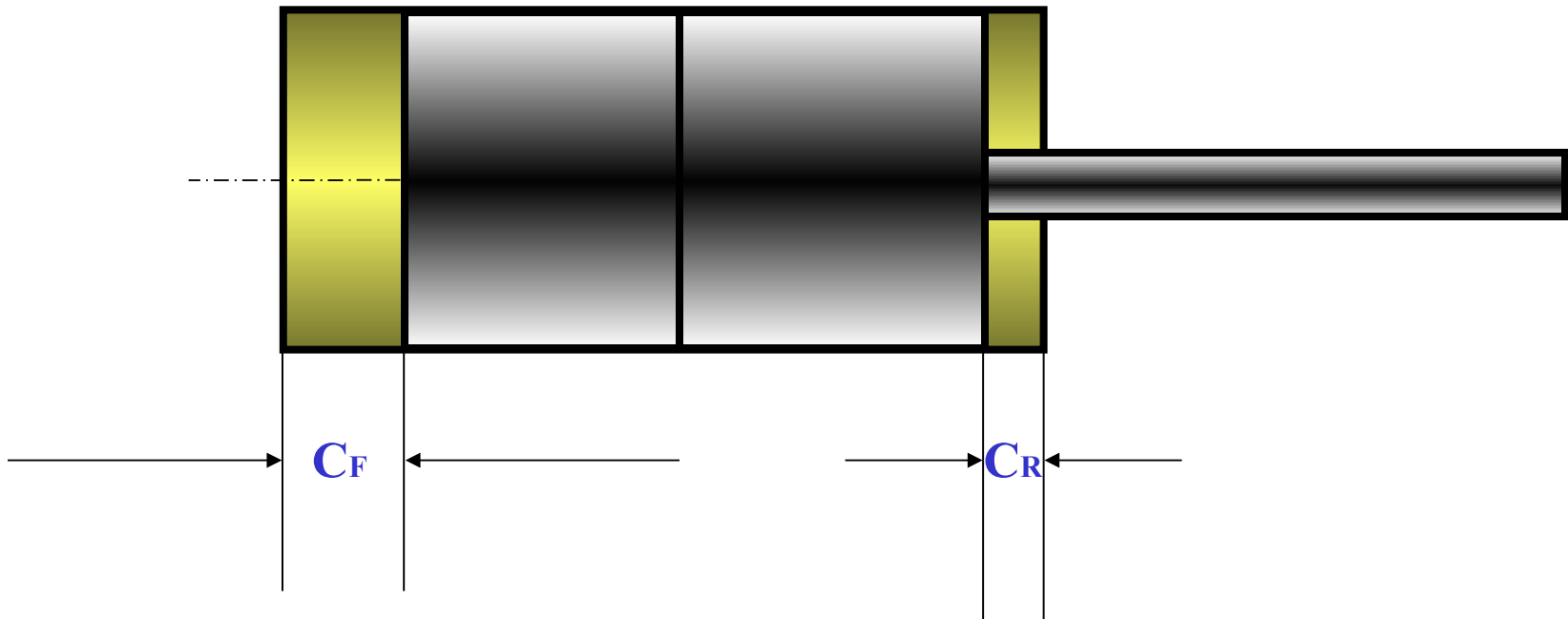
• VARIABLE CLEARANCE

Before operating

$C = \text{Total Clearance Volume} = C_F + C_R$

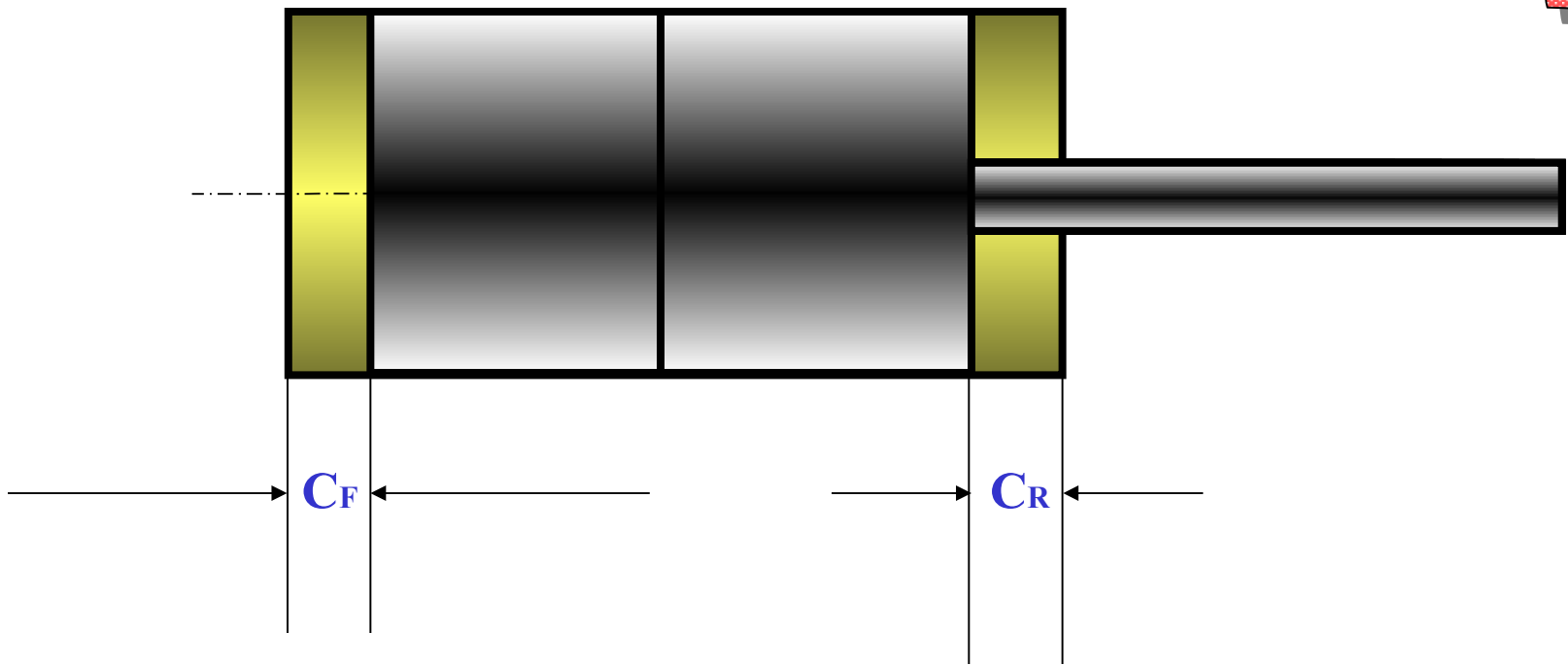
$$C_F = \frac{2}{3} C$$

$$C_R = \frac{1}{3} C$$



After operating

$$C_F = \frac{1}{2} C$$
$$C_R = \frac{1}{2} C$$



EFFECT OF CLEARANCE VOLUME

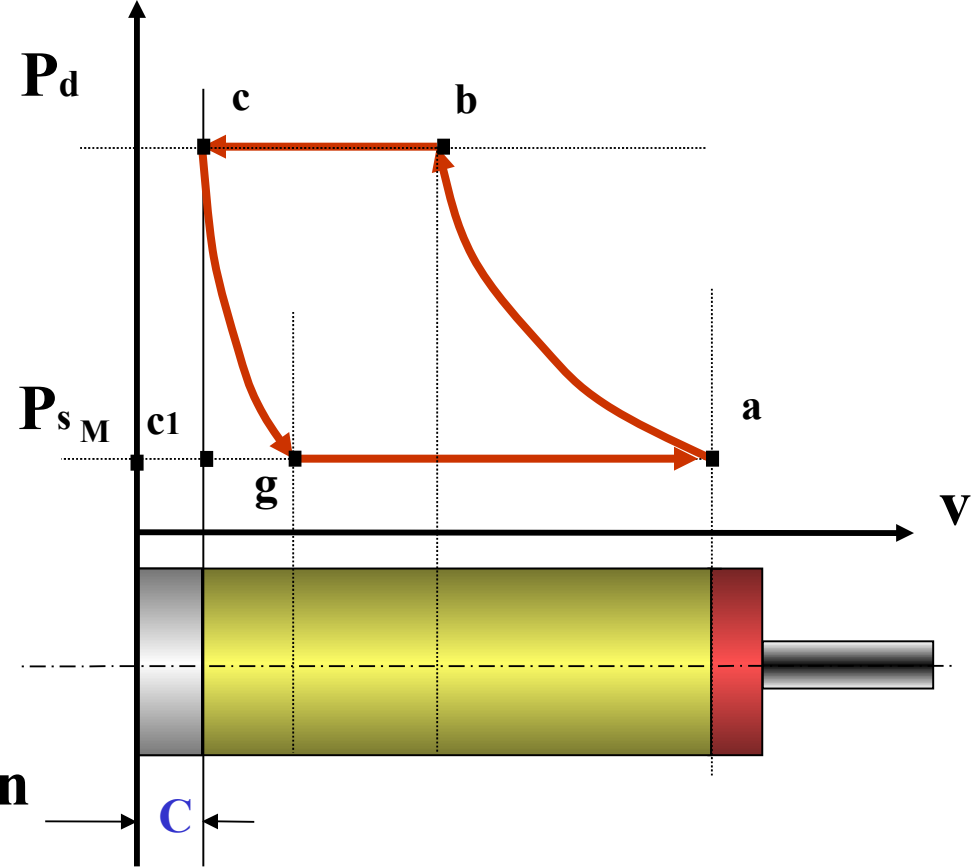
At

Point **a** suction valves closed

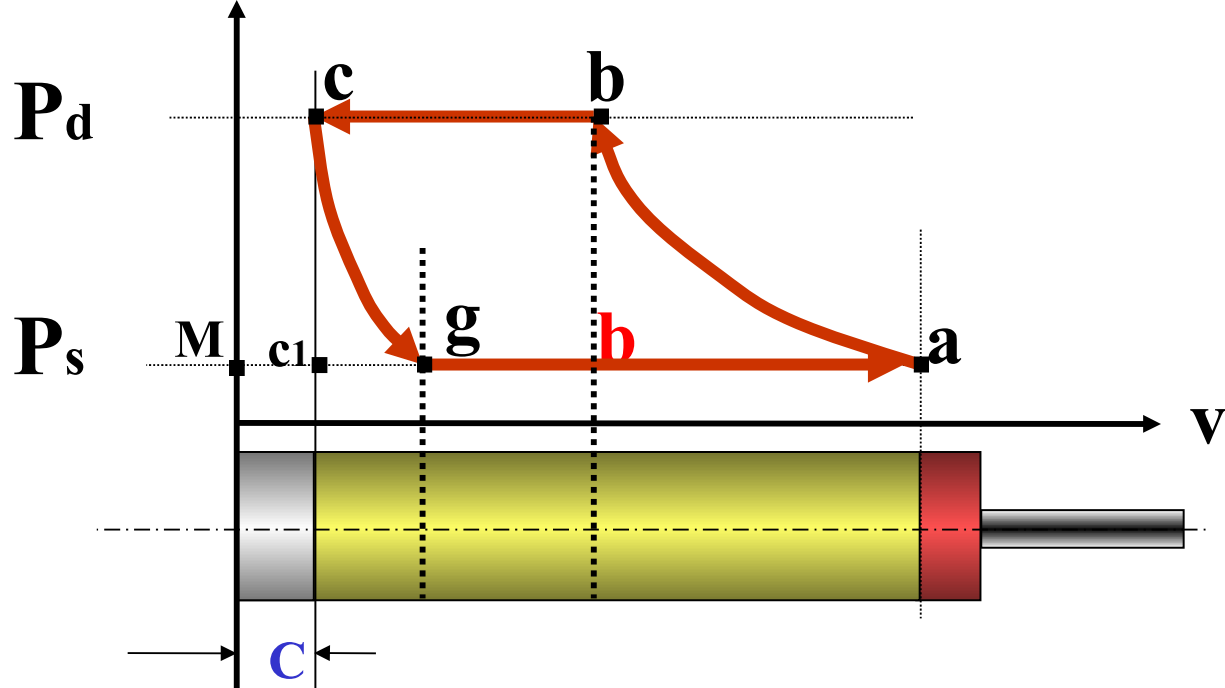
Point **b** discharge valves open

Point **c** discharge valves closed

Point **g** suction valves open



C = Clearance volume



Pressure ratio

$$= \frac{P_d}{P_s} \text{)ABSOLUTE(}$$

Volumetric efficiency

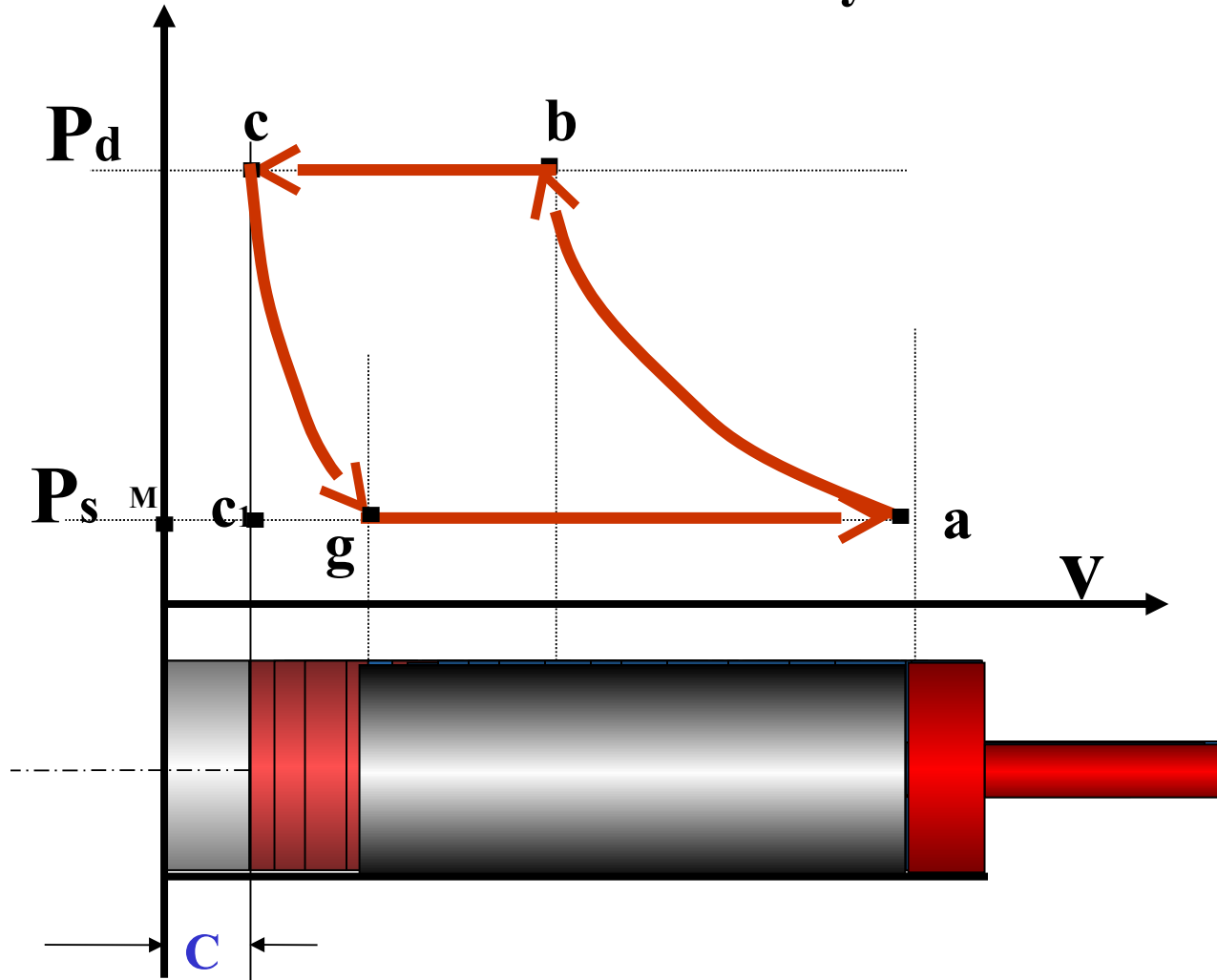
$$= \frac{V_{a g}}{V_{\text{cylinder}}} = \frac{a g}{a M}$$

Compression ratio

$$= \frac{V_{\text{cylinder}}}{V_{b M}} = \frac{a M}{b M}$$

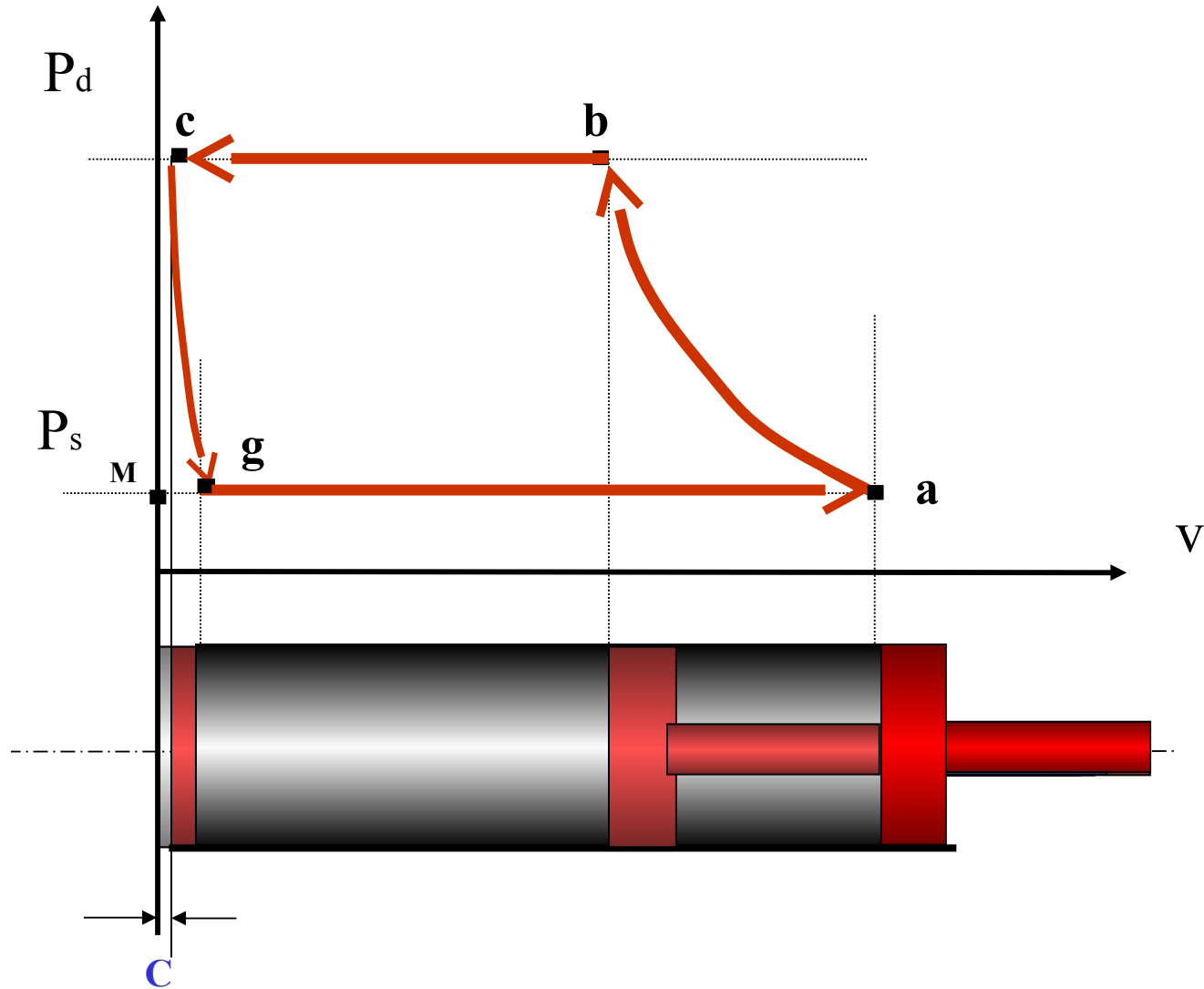
Volumetric efficiency

$$= \frac{V_{a g}}{V_{\text{cylinder}}} = \frac{a g}{a M}$$



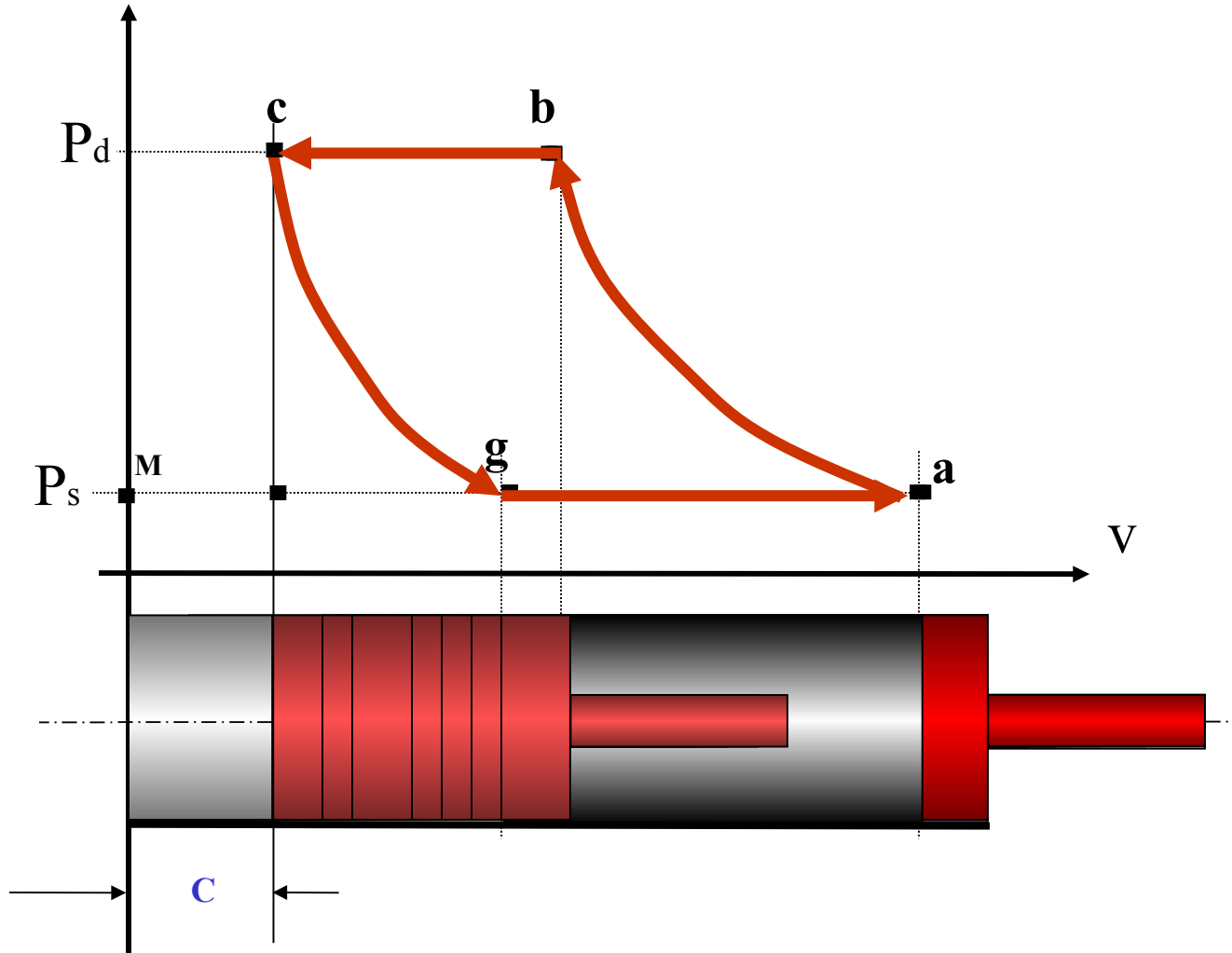
Volumetric efficiency

$$= \frac{V_{a g}}{V_{\text{cylinder}}} = \frac{a g}{a M}$$



Volumetric efficiency

$$= \frac{V_{ag}}{V_{cylinder}} = \frac{ag}{aM}$$



If c increased

suction valves will open at

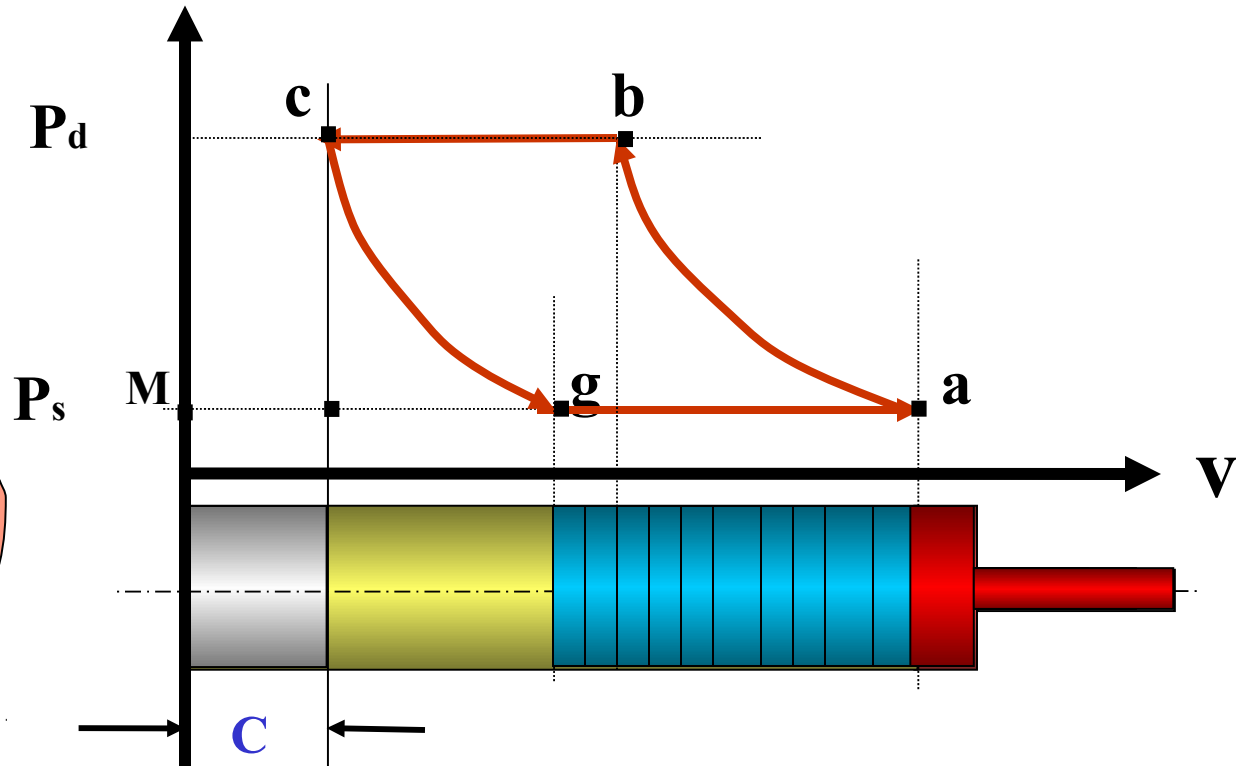
g

Volumetric efficiency

$$= \frac{V_{a g}}{V_{\text{cylinder}}} = \frac{a g}{a M}$$

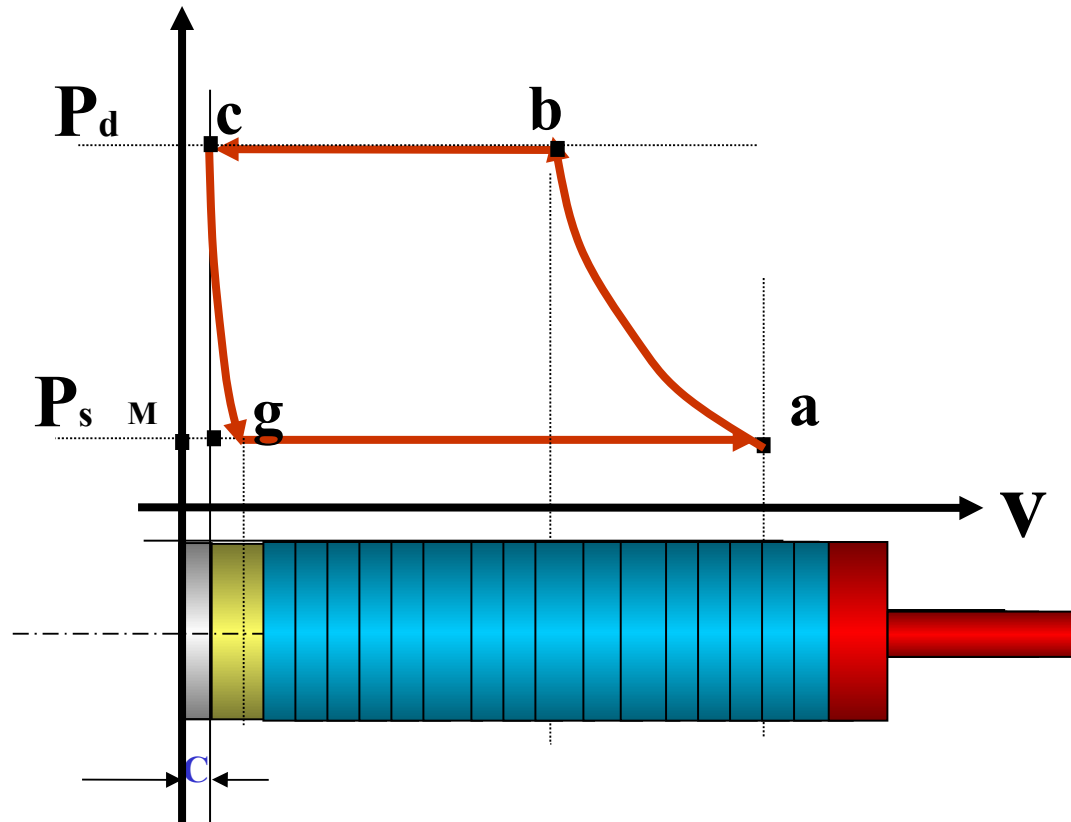
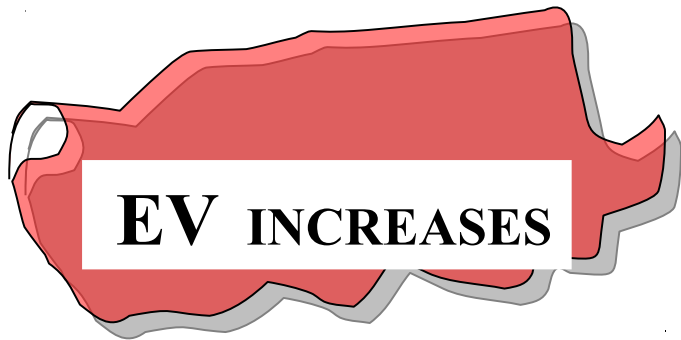
EV DECREASES

Q DECREASES

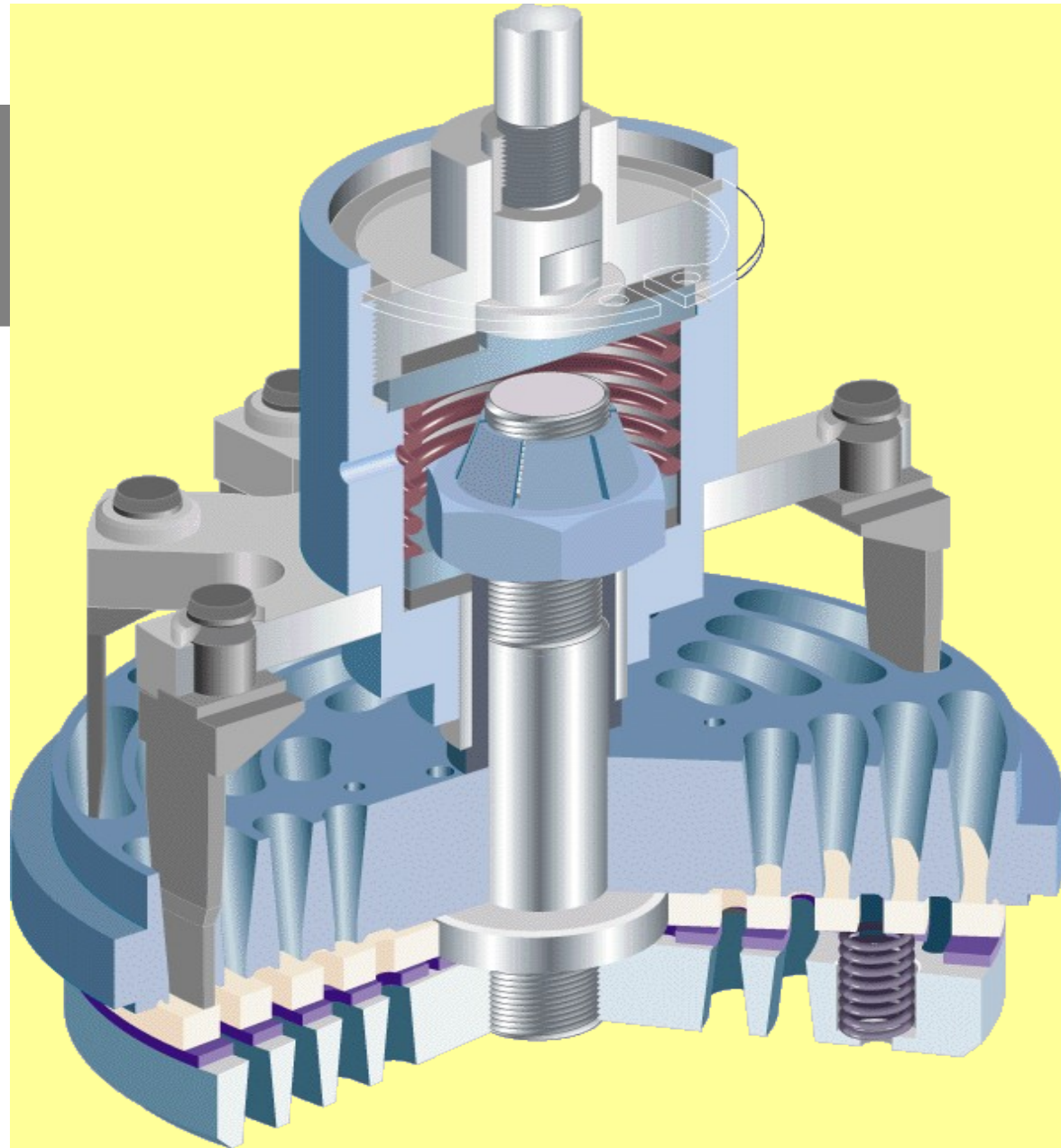


If **c** Decreased suction valves will open at

$$\text{Volumetric efficiency} = \frac{V_{a g}}{V_{\text{cylinder}}} = \frac{a g}{a M}$$



**•SUCTION VALVE
UNLOADERS**



**STUFFING
BOX**

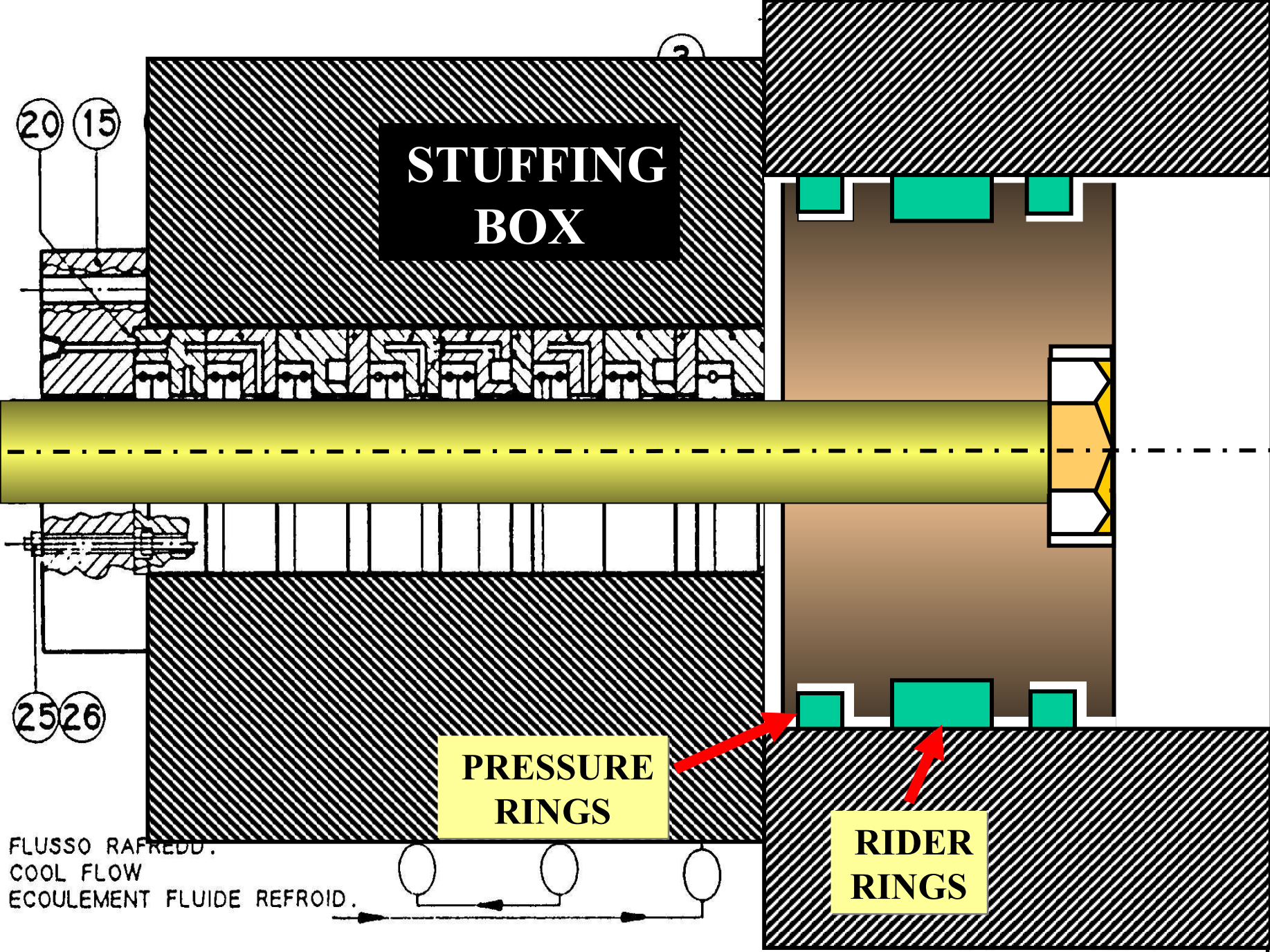
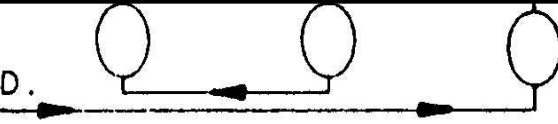
**PRESSURE
RINGS**

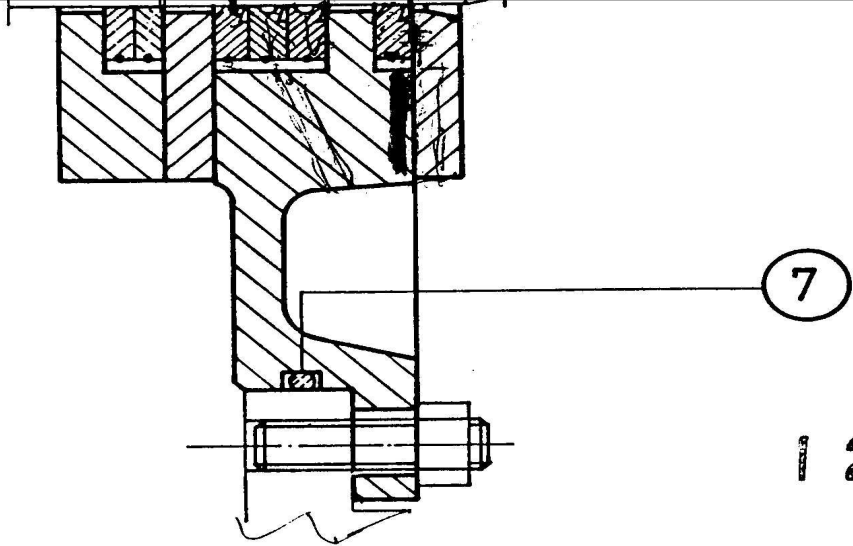
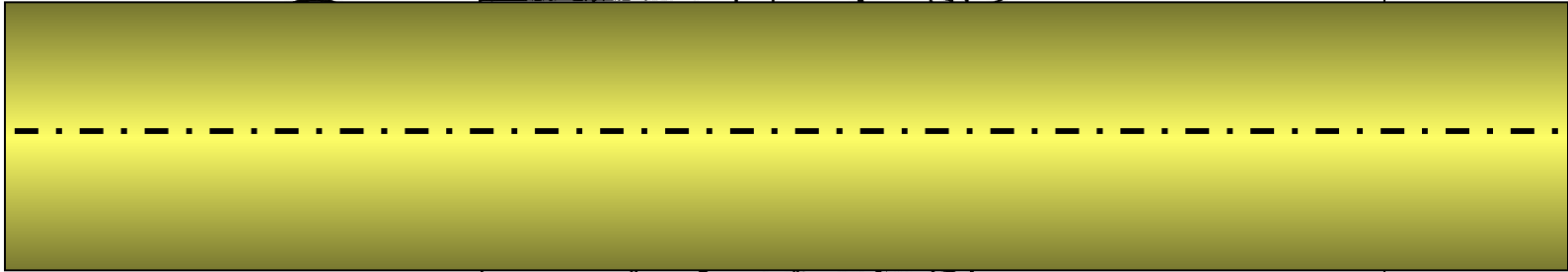
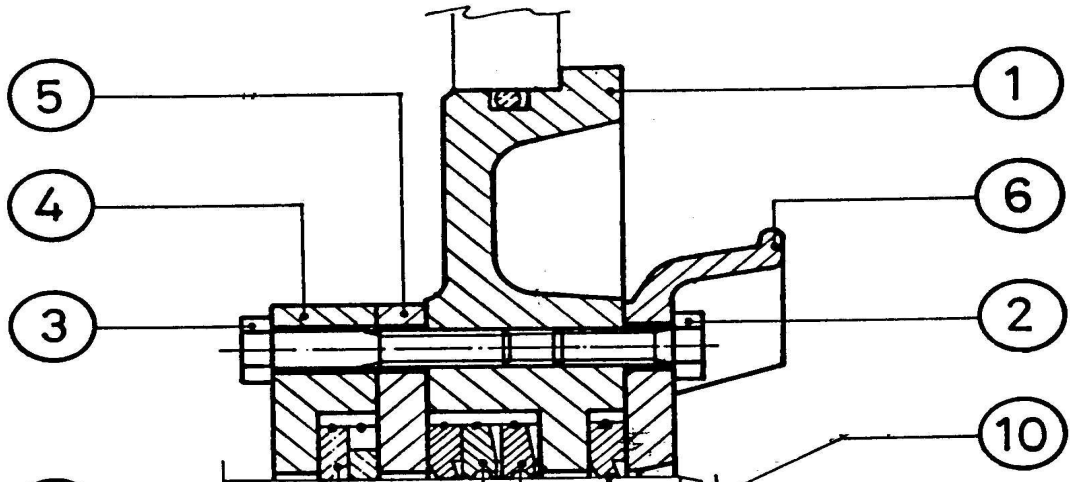
**RIDER
RINGS**

20 15

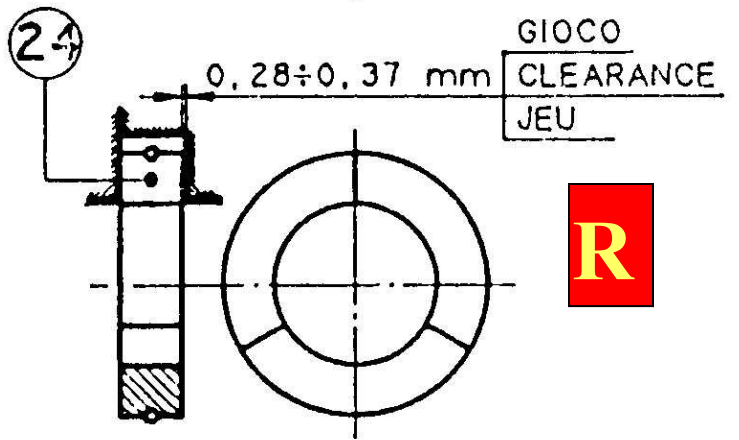
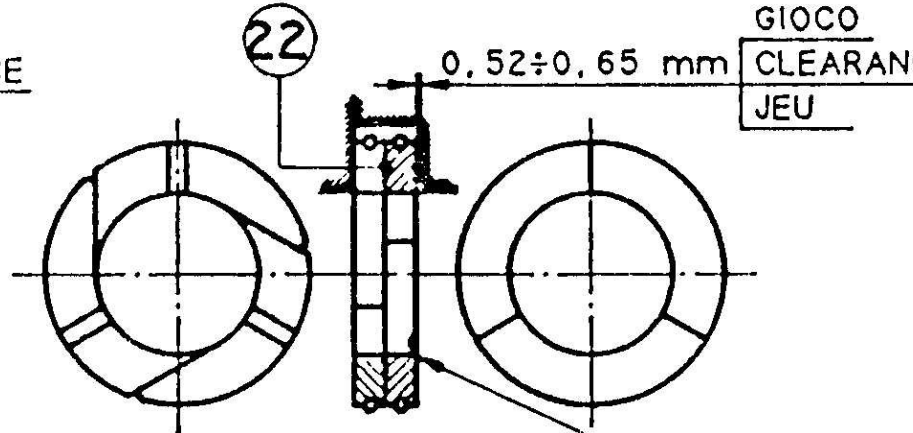
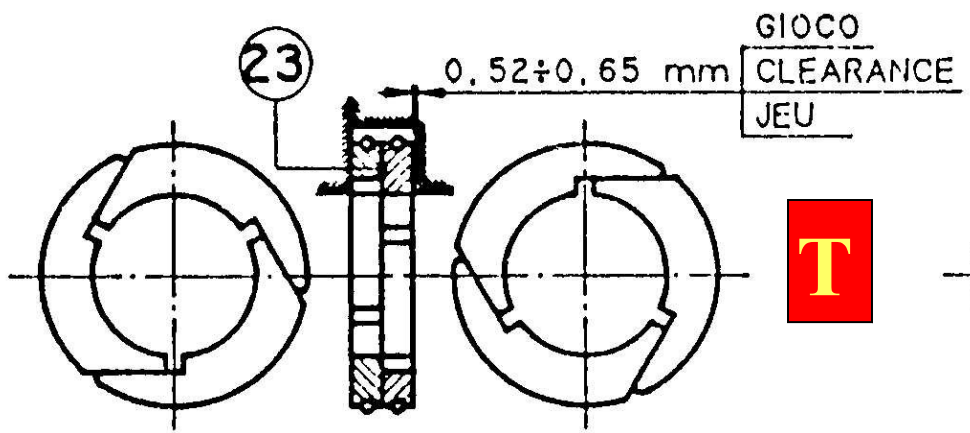
25 26

FLUSSO RAFFREDD.
COOL FLOW
ECOULEMENT FLUIDE REFROID.





**WIPER
RINGS**



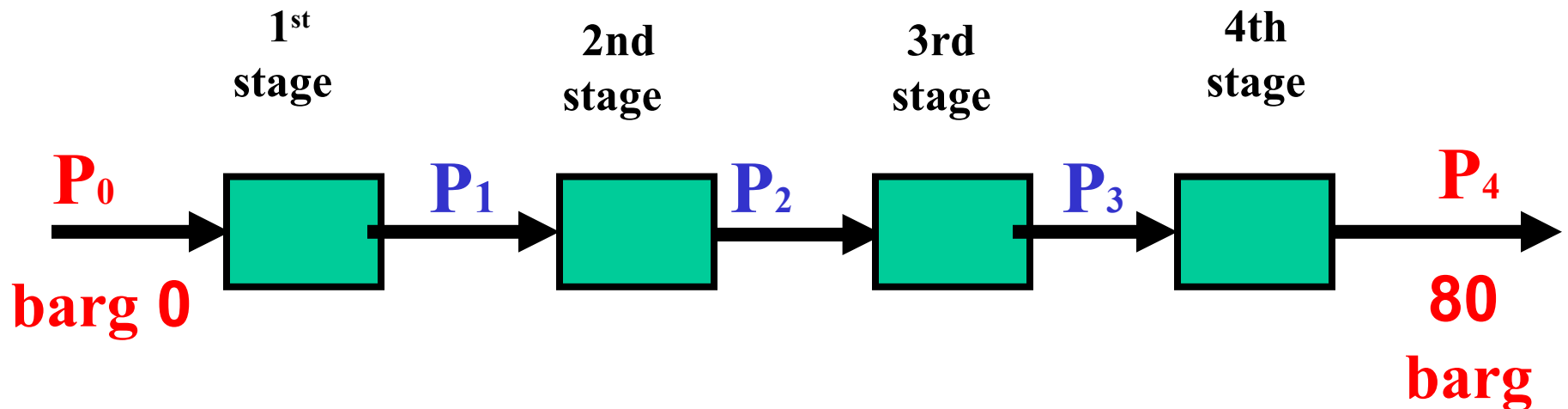
T TANGENTIAL RINGS

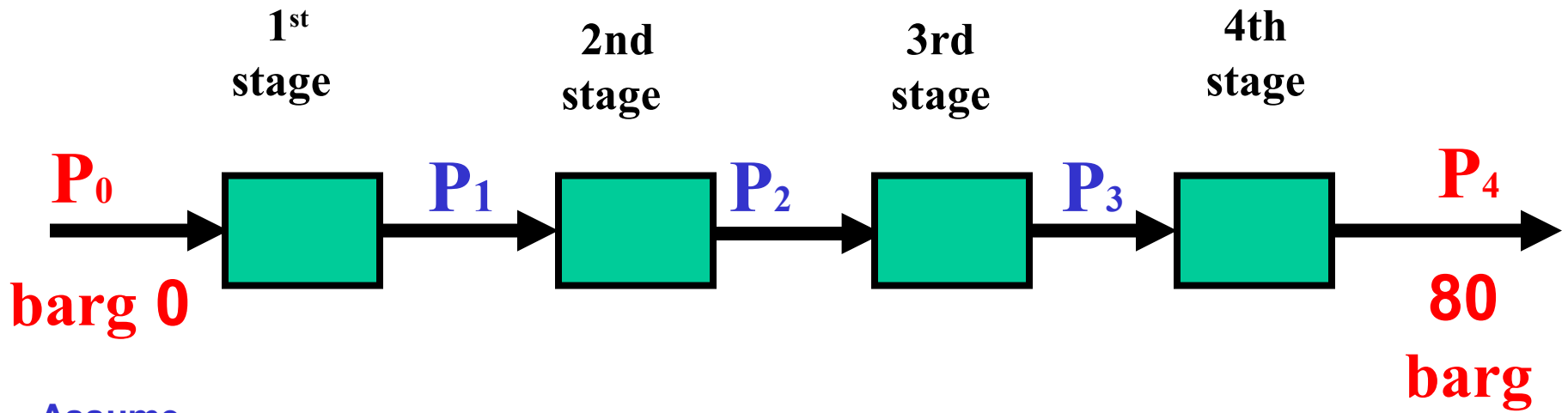
R RADIAL RINGS

**RECIPROCATING
COMPRESSORS
INTERMEDIATE
PRESSURES**

Example 1

Stages Reciprocating Air comp has 4
outlet pressure $P_4 = 80$ barg
what are the intermediate pressures





Assume

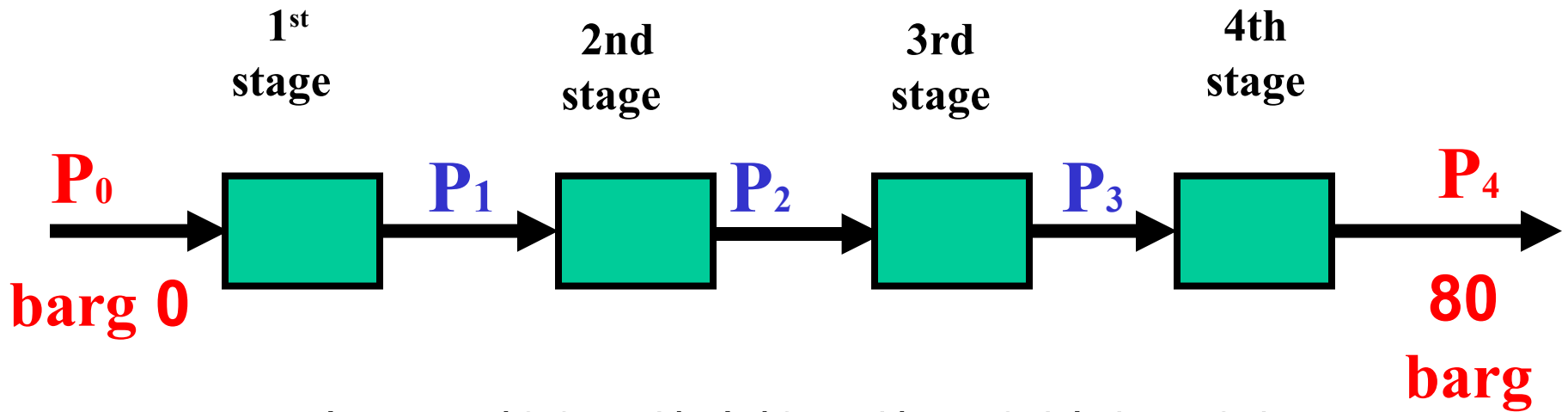
R is The equal Pressure Ratio between stages **AND** $= RT \frac{P_4}{P_0}$

$$= R \frac{P_1}{P_0} = \frac{P_2}{P_1} = \frac{P_3}{P_2} = \frac{P_4}{P_3}$$

$${}^4R \frac{P_4}{P_0} \quad \text{BUT} \quad = RT \frac{P_4}{P_0}$$

Generally

$$\therefore {}^4R = RT \quad \Rightarrow \quad R = \sqrt[4]{RT} \quad \Rightarrow \quad R = \sqrt[N]{RT}$$



$$RT = P_4 / P_0 = (80 + 1) / (0 + 1) = 81 / 1 = 81$$

$$R = \sqrt[N]{RT} = \sqrt[4]{81} = 3$$

$$P_1 = R * P_0 = 3 * 1 = 3 \text{ bara} = 2 \text{ barg}$$

$$P_2 = R * P_1 = 3 * 3 = 9 \text{ bara} = 8 \text{ barg}$$

$$P_3 = R * P_2 = 3 * 9 = 27 \text{ bara} = 26 \text{ barg}$$

$$P_4 = R * P_3 = 3 * 27 = 81 \text{ bara} = 80 \text{ barg}$$

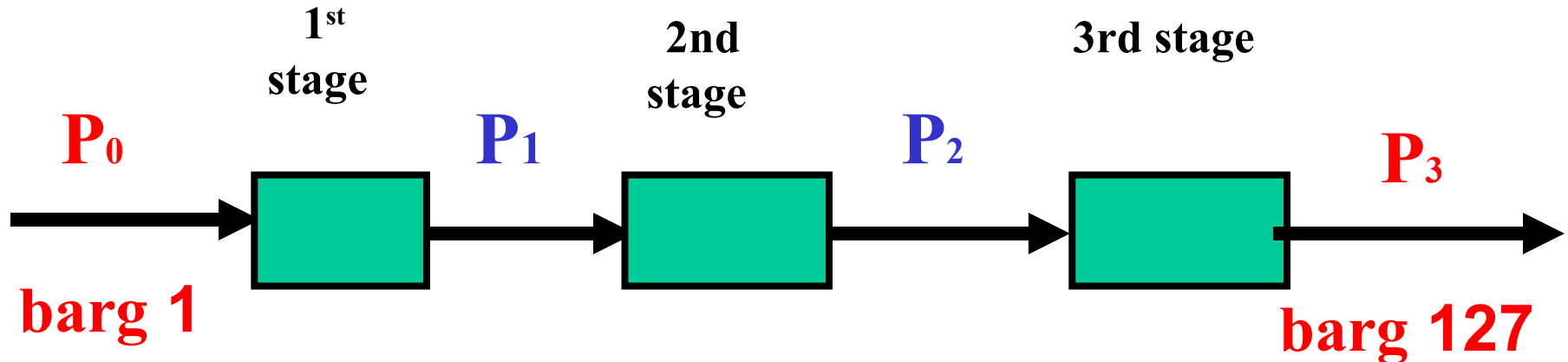
Example 2

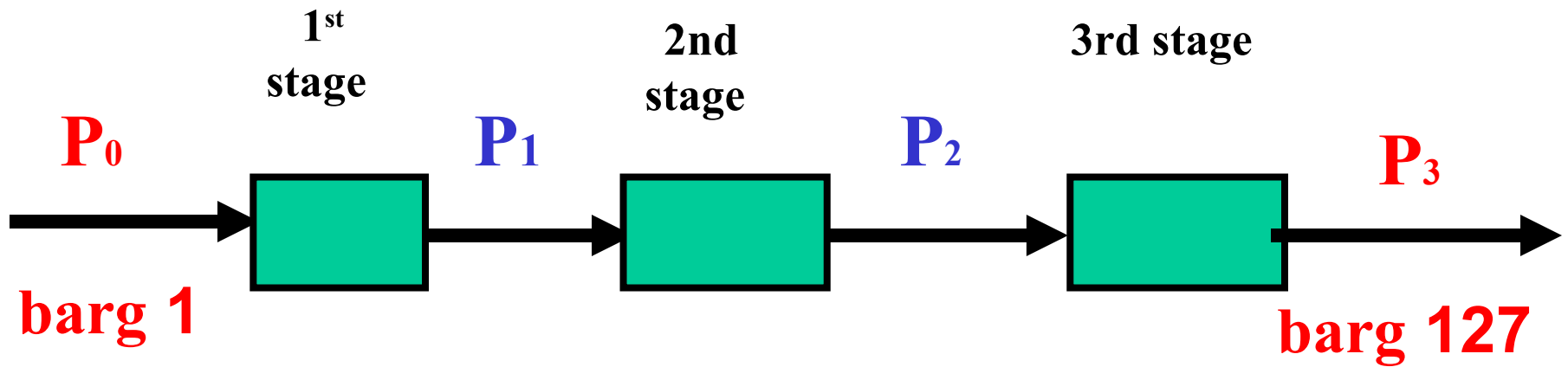
**Stages Reciprocating Gas compressor 3
has**

Outlet pressure $P_3 = 127$ barg

Inlet pressure $P_0 = 1$ barg

what are the intermediate pressures





Assume

$$R = \frac{P_1}{P_0} = \frac{P_2}{P_1} = \frac{P_3}{P_2} \quad \Rightarrow \quad R^3 = \frac{P_3}{P_0}$$

$$RT = \frac{P_3}{P_0} \quad \text{BUT} \quad R^3 = \frac{P_3}{P_0}$$

$$R^3 = RT \quad \Rightarrow \quad R = \sqrt[3]{RT}$$

$$RT = R^3 = \frac{P_3}{P_0} = \frac{(1+127)}{(1+1)} = \frac{128}{2} = 64$$

$$R = \sqrt[3]{RT} = \sqrt[3]{64} = 4$$

$$P1 = R * P0 = 4 * 2 = 8 \text{ bara} = 7 \text{ bar g}$$

$$P2 = R * P1 = 4 * 8 = 32 \text{ bara} = 31 \text{ bar g}$$

$$P3 = R * P2 = 4 * 32 = 128 \text{ bara} = 127 \text{ bar g}$$

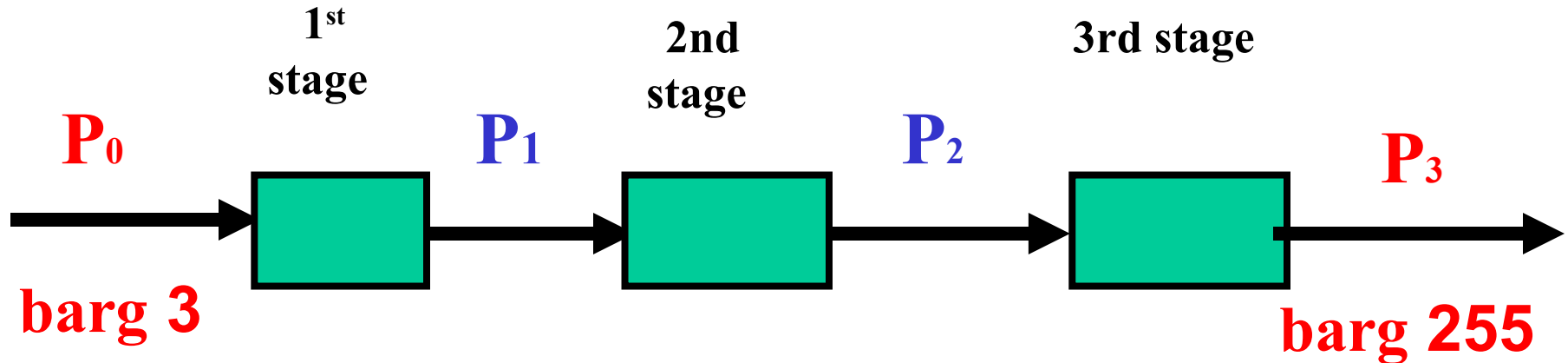
Example 2

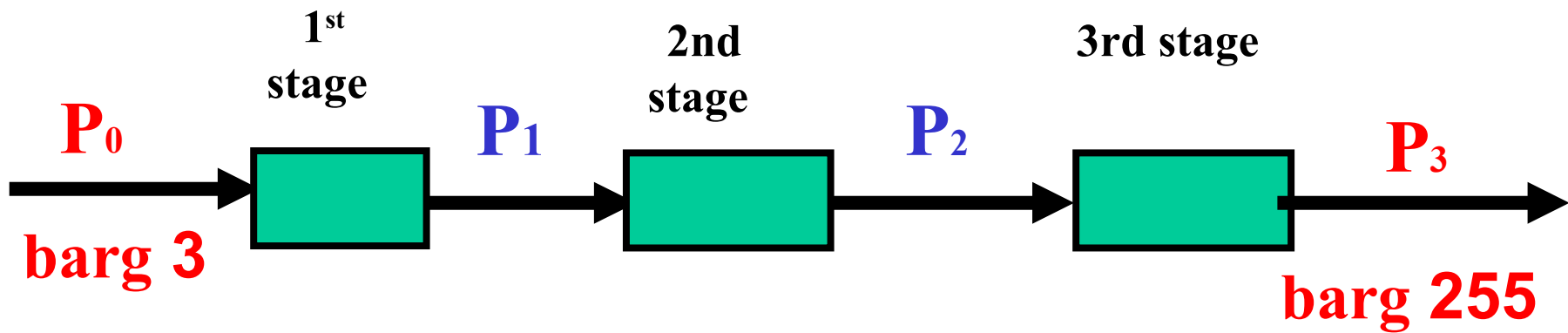
Stages Gas compressor has 3

Outlet pressure = 255 bar g

Inlet pressure = 3 bar g

What are the intermediate pressures





$$RT = R^3 = \frac{P_3}{P_0} = \frac{(1+255)}{(3+1)} = \frac{256}{4} = 64$$

$$R = \sqrt[3]{RT} = \sqrt[3]{64} = 4$$

$$P_1 = R * P_0 = 4 * 4 = 16 \text{ bara} = 15 \text{ bar g}$$

$$P_2 = R * P_1 = 4 * 16 = 64 \text{ bara} = 63 \text{ bar g}$$

$$P_3 = R * P_2 = 4 * 64 = 256 \text{ bara} = 255 \text{ bar g}$$

REFERENCES

1. **L. Nelik.** *Centrifugal and Rotary Pumps: Fundamentals with Applications*, CRC Press, Boca Raton, 1999.
2. **Sulzer Pumps.** *Centrifugal Pump Handbook*, 3rd edition, Sulzer Pumps Ltd., Winterthur, Switzerland, Elsevier, 2010.
3. **S. L. Dixon and C. A. Hall.** *Fluid Mechanics and Thermodynamics of Turbomachinery*, 6th Edition, Elsevier Inc., Amsterdam, 2010.
4. **M. P. Singh and G. M. Lucas.** *Blade Design and Analysis for Steam Turbines*, McGraw-Hill Companies, Inc., 2011.
5. **M. P. Boyce.** *Gas Turbine Engineering Handbook*, 3rd edition, GPM, Houston, Texas, 2005.
6. **C. Soares.** *Microturbines: Applications for Distributed Energy Systems*, Elsevier, Amsterdam, 2007.
7. **A. S. Leyzerovich.** *Wet-Steam Turbines for Nuclear Power Plants*, PennWell Corporation, Tulsa, Oklahoma, 2005.
8. **S. Yedidiah.** *Centrifugal Pump User's Guidebook: Problems and Solutions*, Chapman & Hall, New York, 1996.
9. **M. L. Adams Jr.** *Power Plant Centrifugal Pumps Problem Analysis and Troubleshooting*, CRC Press, Boca Raton, 2017.