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LAMPIRAN 1

Dalam perhitungan perancangan alat distilasi menggunakan contoh jurnal berjudul "Pengambilan minyak atsiri dari daun dan batang sereh wangi menggunakan metode distilasi uap air dengan pemanasan *microwave*". Dapat diketahui yaitu :

Massa bahan = 2,5 kg cengkeh = 2500 gram

Suhuoperasi (T) = 105⁰C

Tekanan (P) = 1 atm

Waktu = ±2 jam

Pelarut (air) = 2 liter

% rendemen = 0,29% - 1,52%

Densitas = 0,872 - 0,882 gr/cm³

Indeks bias = 1,415 - 1,472

Bilangan asam = 2,805 - 3,366

Penyelesaian :

Menghitung kolom diameter (Kapasitas)

$$\text{Gas flow rate} = \frac{\text{Massa Benda}}{\text{Waktu}}$$

$$= \frac{2,5 \text{ kg}}{1 \text{ h}} = 2,5 \text{ kg/h}$$

$$= \frac{2,5 \text{ kg/h}}{29 \text{ mol}} = 0,086 \text{ kmol/h}$$

$$\text{Liquid flow rate} = \frac{29,0}{\% \text{ Rendemen}}$$

$$= \frac{29,0}{0,29 \%} \times 0,086 \text{ kmol/h}$$

$$= 8,6 \text{ kmol/h} \times 17,9885$$

$$= 154,671 \text{ kg/h} = \frac{154,671 \text{ kg/h}}{3600 \text{ s}} = 0,00819 \text{ kg/s}$$

Select 38mm (1½ in) ceramixintalax Saddles, $F_p = 52$ (From table 11.2)

$$\text{Gas density at } 105^\circ\text{C} = \frac{29}{\text{Ketetapan}} \times \frac{273^\circ\text{F}}{\text{Suhu bahan } (^\circ\text{F})}$$

$$= \frac{29}{22,4} \times \frac{273^\circ\text{F}}{(105+273)^\circ\text{F}}$$

$$= 0,935 \text{ kg/m}^2$$

$$\text{Liquid density} = 1000 \text{ kg/m}^3$$

$$\text{Liquid viscosity} = 10^{-3} \text{ Ns/m}^3$$

$$\frac{Lw^*}{Gw^*} \sqrt{\frac{\rho v}{\rho L}} = \frac{154,671}{2,5} \sqrt{\frac{0,935}{10^3}}$$

$$= 1,89$$

Design for a pressure drop of 20 mm H₂O/m packing (Dari buku *Chemical Engineering* halaman 495)

$$K_4 = 0,35 \text{ (From table 11.4)}$$

At Flooding $K_4 = 0,8$

$$\% \text{ Flooding} = \sqrt{\frac{0,35}{0,8}} \times 100\%$$

$$= 66 \%$$

$$\text{From table 11.18} \quad V_{w^*} = \left[\frac{K_4 \rho v (\rho v - \rho L)}{42,9 F \rho \left(\frac{\mu L}{\rho L}\right)^{0,1}} \right]^{1/2}$$

$$= \left[\frac{0,35 \times 0,935 (1000 - 0,935)}{42,9 \times 52 \left(\frac{10^{-3}}{10^3}\right)^{0,1}} \right]^{1/2}$$

$$= \left[\frac{326,94}{69,69} \right]^{1/2}$$

$$= 2,167 \text{ kg/m}^2\text{h}$$

$$\text{Column area required} = \frac{2,5}{1,89} = 1,32 \text{ m}^2 \text{ (dibulatkan menjadi 1,5 m)}$$

$$\text{Diameter} = \sqrt{\frac{4}{\pi}} \times \text{column area required}$$

$$= \sqrt{\frac{4}{3,14}} \times 1,32$$

$$= 1,29 \text{ m (dibulatkan menjadi 1,3 m)}$$

$$\text{Column area} = \frac{\pi}{4} \times 1,29^2$$

$$= 1,30 \text{ m}$$

$$\text{Packing size to column diameter ratio} = \frac{1,3}{38 \times 10^{-3}}$$

$$= 34$$

$$\% \text{ Flooding at selected diameter} = \% \text{ flooding} \times \frac{\text{diameter}}{\text{colom area}}$$

$$= 66 \times \frac{1,29}{1,3}$$

$$= 65 \%$$

Clod consider reducing column diameter estimations of Hob

- Cornell's method

$$DL = 1,7 \times 10^{-9} \text{ m}^2/\text{s}$$

$$Dv = 1,45 \times 10^{-5} \text{ m}^2/\text{s}$$

$$\mu v = 0,018 \times 10^{-3} \text{ Ns/m}^2$$

$$(\text{Sc})_v = \frac{0,081 \times 10^{-3}}{0,935 \times 1,45 \times 10^{-3}}$$

$$= 1,27$$

$$(Sv) = \frac{10^{-3}}{1000 \times 1,7 \times 10^{-9}}$$

$$= 588$$

$$Lw^* = \frac{154,671}{1,30}$$

$$= 118,9 \text{ kg/m}^2\text{h} \rightarrow : 3600 \text{ (s)} = 0,033 \text{ kg/m}^2$$

- From fig. 11.41 at Gs percent flooding ,k3 = 0,79
- From fig 11.42 at Gs percent flooding = 57
- From fig 11.48 at Lw* = 0,033, $\phi n = 0,01$

Cornell's method

Persamaan 11.11

$$HL = 3,05 \phi n (Sc) l 0,5 k3 \frac{z}{3,05} \cdot 0,15$$

Size 50 (2 in) mm , HETP, in 0,9m

$$HL = 0,35 \times 0,01 (588)^{0,5} \times 0,79 \frac{0,9}{3,05}$$

$$HL = 0,028 \text{ M}$$

$$HG = 0,11 \times 57 (1,27)^{0,5} (2.3) \frac{0,9^{0,33}}{3,05} / (0,033)^{0,5}$$

$$HG = 0,67 \text{ m}$$

Dibutuhkan menjadi = 0,7m

Optimumnya antara 0,6 sampai 0,8 diambil 0,7

Persamaan 11.105

$$HOG = Hg + \frac{m6 \ m}{Lm} H_2$$

$$HOG = 0,67 + 0,7 \times 0,028$$

$$= 0,68 \text{ m}$$

$$Z = 0,9 \times 0,7 = 0,63 \text{ m}$$

Nilai tinggi (higher) dengan menggunakan metode cornell's didapatkan sekitar = 0,63 m

LAMPIRAN 2

PERHITUNGAN % HASIL RENDEMEN MINYAK ATSIRI KUNYIT

% RENDEMEN PADA AMPAS KUNYIT

$$\% \text{ Rendemen} = \frac{\text{jumlah minyak yang dihasilkan}}{\text{jumlah bahan sebelum diolah}} \times 100\%$$

$$\% \text{ Rendemen} = \frac{15,74-14,88}{4000} \times 100\% = 0,0215$$

$$\% \text{ Rendemen} = \frac{16,34-14,88}{4000} \times 100\% = 0,0365$$

$$\% \text{ Rendemen} = \frac{16,98-14,88}{4000} \times 100\% = 0,0215$$

% RENDEMEN PADA RIMPANG KUNYIT

$$\% \text{ Rendemen} = \frac{\text{jumlah minyak yang dihasilkan}}{\text{jumlah bahan sebelum diolah}} \times 100\%$$

$$\% \text{ Rendemen} = \frac{15,78-14,88}{4000} \times 100\% = 0,0225$$

$$\% \text{ Rendemen} = \frac{16,43-14,88}{4000} \times 100\% = 0,03875$$

$$\% \text{ Rendemen} = \frac{16,95-14,88}{4000} \times 100\% = 0,05175$$