



*Original Article*

## Impact of hazardous components on CO<sub>2</sub> biofixation from synthetic flue gas using *Chlorella sp.* JPR-1 in a raceway pond photobioreactor

Andri Cahyo Kumoro\*, Hadiyanto, and Heru Susanto

*Department of Chemical Engineering, Faculty of Engineering,  
Diponegoro University, Prof. H. Soedarto, SH Road, Tembalang-Semarang, 50275 Indonesia.*

Received 30 January 2012; Accepted 14 June 2013

---

### Abstract

This work aimed to investigate the effects of hazardous compounds (NO and SO<sub>2</sub>) in flue gas on *Chlorella* JPR-1 growth in a raceway pond photobioreactor at ambient temperature (30 °C) without pH control. *Chlorella* JPR-1 exhibited its tolerant to CO<sub>2</sub> content in the flue gas as high as 50%. The maximum carbon fixation rate (1.84 g CO<sub>2</sub>/L.day) observed when the flue gas contained 10% CO<sub>2</sub>. Although the specific growth rate was 25.88% lower than the control culture when cultivated with 50 ppm SO<sub>2</sub>, *Chlorella* JPR-1 still could grow when cultured with 100 ppm SO<sub>2</sub> with slightly longer lag phase period. A growth rate reduction of 3.53% of the control culture was observed when *Chlorella* JPR-1 was cultured with flue gas containing 50 ppm NO. This study has shown that *Chlorella* JPR-1 has a high potential to be used for CO<sub>2</sub> fixation from flue gas.

**Keywords:** fixation, CO<sub>2</sub>, SO<sub>2</sub>, NO, microalgae, specific growth rate

---

### 1. Introduction

The increase of the atmospheric greenhouse gas (CO<sub>2</sub>) concentration due to combustion is considered to be one of the main causes of global warming (e.g. Malhi *et al.*, 2002). Within the last 10 years, the CO<sub>2</sub> gas emission in Indonesia has significantly increased from 100 to 380 Mt (Mega ton) CO<sub>2</sub> per year, and it is estimated that in 2020 the CO<sub>2</sub> emission will reach 684 Mt CO<sub>2</sub> ([www.dirgantara-lapan.or.id](http://www.dirgantara-lapan.or.id)). Therefore, the reduction of CO<sub>2</sub> emission becomes an inevitable issue. Many approaches have been adopted to limit and reduce CO<sub>2</sub> emissions. These include enhancing energy production efficiency, substituting carbon-rich fossil fuels such as coal and oil, with natural gas and other less carbon or carbon-free energy sources, and developing technologies to capture CO<sub>2</sub> in view of reutilization and/or sequestration.

The CO<sub>2</sub> captures can be performed by physical and chemical absorption methods (Dugas and Rochelle, 2009), cryogenic and membrane separations, and biofixation (Wang *et al.*, 2008).

The CO<sub>2</sub> biofixation approaches have drawn much attention because they lead to the production of biomass energy through photosynthesis by autotrophic organisms. Microalgae offer several advantages over the terrestrial energy crops, including higher photosynthetic efficiency, growth rates and biomass production (Gouveia and Oliveira, 2009). Microalgae can fix CO<sub>2</sub> from different sources, which can be categorized as CO<sub>2</sub> from the atmosphere, CO<sub>2</sub> from industrial and transportation exhaust gases, and fixed CO<sub>2</sub> in the form of soluble carbonates (Wang *et al.*, 2008). One of the other advantages is that a number of microalgae strains have the ability to store large quantities of lipids, which varied from 1 to 26 % (Allard and Templier, 2000). This fact has attracted great attention from researchers around the world to investigate the potential of marine microalgae as the main oil source for biodiesel production (Gavrilescu and Chisti, 2005; Metzger and Largeau, 2005).

---

\* Corresponding author.

Email address: [andrewkomoro@undip.ac.id](mailto:andrewkomoro@undip.ac.id)

Direct use of flue gas in microalgae culture may reduce the cost of pretreatment. However, the presence of algal growth inhibitors in the raw flue gas, such as  $\text{SO}_x$  and  $\text{NO}_x$ , would be very critical as an addition to the high concentrations of  $\text{CO}_2$  (Silva and Pirt, 1984). Yoshihara *et al.* (1996) found that at higher cell concentration in the culture, marine microalga strain NOA-113 exhibited higher tolerance to  $\text{NO}$ . From their study, Yanagi *et al.* (1995) reported that *Chlorella* HA-1 was not inhibited by 50 ppm  $\text{NO}$ , but the strain could not grow with the presence of 50 ppm  $\text{SO}_2$ . Kurano *et al.* (1995) investigated the tolerances of three algal strains, *C. caldarium*, *Galdieria partita* and *Cyanidioschyzon melorae*, isolated from a hot water spring, to  $\text{NO}$  and  $\text{SO}_2$ , and reported that all of the strains showed good growth at 50 ppm  $\text{NO}$  aeration but only *G. partita* could proliferate under 50 ppm  $\text{SO}_2$  aeration. Later, Hauck *et al.* (1996) reported that microalga *Cyanidium caldarium* exhibited some growth in a simulated flue gas containing about 200 ppm of  $\text{SO}_2$  for the first 20 hrs, but the growth of *Chlorella vulgaris* was completely inhibited. This toxic effect may be due to either a lowering of the pH of the culture medium or direct inhibition by the  $\text{SO}_2$  itself (Hauck *et al.*, 1996). Considering that actual flue gas from industrial sources contains about 100-300 ppm  $\text{NO}_x$  and  $\text{SO}_x$  (Yoshihara *et al.*, 1996), algal strains reported in the literature could not be used for direct  $\text{CO}_2$  fixation from flue gas. Recently, Sung *et al.* (1998) isolated a fast growing alga in  $\text{CO}_2$  enriched condition which could grow well in up to 20%  $\text{CO}_2$ . In the present study, the effects of  $\text{SO}_2$  and  $\text{NO}$  on growth of *Chlorella* JPR-1 have been investigated to determine the feasibility for the direct  $\text{CO}_2$  fixation process from actual flue gas.

## 2. Materials and Methods

### 2.1 Microorganism and growing medium

*Chlorella* JPR-1, a highly  $\text{CO}_2$  tolerant and fast growing microalgae, isolated from marine water collected from Teluk Awur Marine Life Laboratory was used in this study. The strain was kept on Detmer agar plate, and cultured on a modified M4N medium. The composition of the medium and the preparation procedure was similar to that used by Sung *et al.* (1998). Although Hirata *et al.* (1996) reported that *C. vulgaris* is best grown at  $30^\circ\text{C}$  and pH 5.5 to 6.0, the initial pH of the medium used in this work was 5.5, with no further adjustment was made. This is because it is possible to cultivate algae using wastewater nutrients and the  $\text{CO}_2$  present in the flue gases without buffering or pH control (Yun *et al.*, 1996), and the fact that buffering is not a practical option for pH control in large cultivation systems.

### 2.2 Culture experiments

The microalgae culture experiments were conducted to determine the tolerances of *Chlorella* JPR-1 to  $\text{CO}_2$ ,  $\text{SO}_2$  and  $\text{NO}$  in various gas mixtures using a  $0.4 \text{ m}^3$  raceway pond

bioreactor (Figure 1). Typical flue gas emitted from a boiler using low-sulfur heavy oil as fuel contains 10-15%  $\text{CO}_2$  and 100-300 ppm  $\text{NO}_x$  and  $\text{SO}_x$  (Sung *et al.*, 1998). Therefore, several synthetic gas mixtures containing various concentrations of  $\text{CO}_2$ ,  $\text{SO}_2$ , and  $\text{NO}$ , were used for the experiments to evaluate the effects of the inhibitory compounds on growth of *Chlorella* JPR-1. The growth rates were monitored with different gas mixtures which contained different concentrations of  $\text{CO}_2$ ,  $\text{SO}_2$  and  $\text{NO}$ . The seed culture was centrifuged and washed before inoculation. Samples were removed intermittently from the vessels to determine the cell concentration for further algal growth calculation. The temperature of the culture media was maintained at local ambient temperature ( $30^\circ\text{C}$ ). The gas flow rate was measured with a flow meter (Dewyer, U.S.A.) and fixed to 0.5 volume gas/volume liquid/min. Air-grown cells were inoculated into the medium to obtain the initial cell concentration specified in the experimental results.

### 2.3 Microalgal carbon content, cell counting, and dry weight analysis

Biomass carbon content was determined using a Perkin-Elmer 2400 CHNS (carbon, hydrogen, nitrogen, and sulfur) element analyzer calibrated to the 100% value using a certified cystine standard (Perkin-Elmer, U.S.A.) (de Moraes and Costa, 2007).

A direct microscopic count (cells  $\text{mL}^{-1}$ ) was performed on a sample of microalgal suspension using a Bürker-Türk

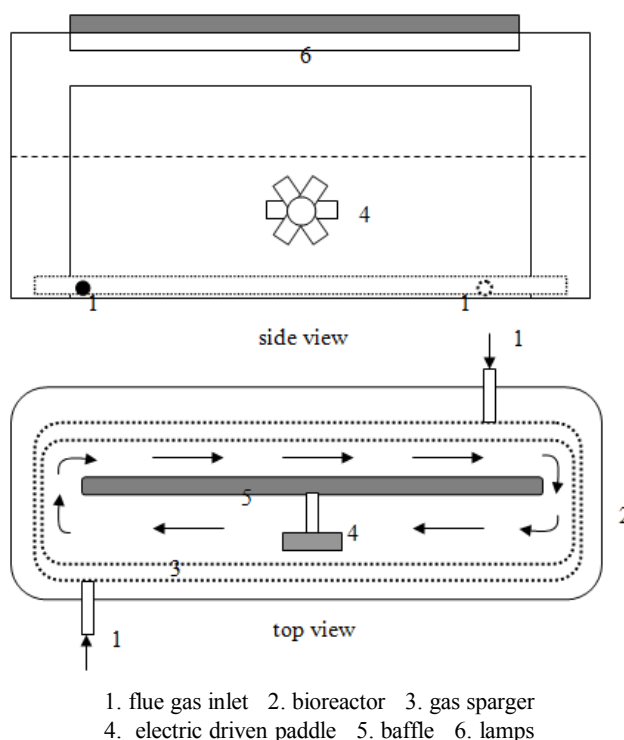


Figure 1. Raceway pond bioreactor used for *Chlorella* sp. JPR-1 culture.

counting chamber (Brand, Germany) and a Nikon Eclipse 80i microscope (Nikon Corporation, Japan). Optical density of the microalgal suspension was measured by absorbance at 550 nm ( $A_{550}$ ) in an HP 8452 UV/Visible Spectrophotometer. The spectrophotometer was blanked with each medium. At the end of the experiments, 100 mL of the culture broth was removed from every flask, respectively. The samples were filtered through glass microfibre discs (Sartorius stedim biotech, Göttingen, Germany) and the dry weights of pellets were measured after drying at 105°C for 2 hrs.

## 2.4 Microalgae growth rate

The algal growth rate was determined in the linear growth phase because most of the algal growth occurred during this phase (Yun *et al.*, 1997). The specific growth rate,  $m$ , (1/day), which is a measure of the number of generations (the number of doublings) that occur per unit of time in an exponentially growing culture of the *Chlorella* JPR-1 was then evaluated using the following equation (Lee and Shen, 2004):

$$\mu = \frac{\ln(x_2) - \ln(x_1)}{t_2 - t_1} \quad (1)$$

where  $x_2$  and  $x_1$  are biomass concentrations (g/L) after  $t_2$  and  $t_1$  day cultivation, respectively.

## 2.5 Carbon dioxide fixation rate

The  $\text{CO}_2$  fixation rate,  $R_c$ , (g/L.day), was calculated from an elemental analysis of the algal biomass, as shown in Equation 2 (Zheng *et al.*, 2011):

$$R_c = C_c \times \left( \frac{x_2 - x_1}{t_2 - t_1} \right) \times \frac{MCO_2}{MC} \quad (2)$$

Where  $C_c$  is the carbon content of the biomass and  $MCO_2$  and  $MC$  are the molecular weight of  $\text{CO}_2$  and carbon, respectively.

## 3. Results and Discussion

The effects of  $\text{CO}_2$  concentrations on growth of *Chlorella* JPR-1 are illustrated in Figure 2 and 3. *Chlorella* JPR-1 was cultured under continuous illumination with different concentrations of  $\text{CO}_2$  in the flue gas ranging from 10 to 50% (v/v). The curves of microalgae cells concentration in the cultivation pond presented in Figure 2 show that the concentration of  $\text{CO}_2$  in the flue gas affects the growth rate of *Chlorella* JPR-1. This finding is similar to the growth of *C. vulgaris* reported by Yun *et al.* (1996). The fastest growth was achieved in the culture medium with 10%  $\text{CO}_2$  concentration in the flue gas supply. However, the cells still can survive till  $\text{CO}_2$  concentration in the flue gas up to 50%. The maximum biomass concentration reached by introduction of 10%  $\text{CO}_2$  was 5.8 g/L, and it decreased significantly

by increasing the  $\text{CO}_2$  concentration. This result is in accordance with Sung *et al.* (1998) who grew *Chlorella* sp. JKR-1 in a culture with different concentrations of  $\text{CO}_2$  ranging from air-level to 70% and obtained optimum growth rate at 10%  $\text{CO}_2$ . They also reported that *Chlorella* sp. JKR-1 maintained high growth rates and cell concentrations at high  $\text{CO}_2$  concentrations of 30 % and 50 %, but the growth rate became remarkably low at 70%  $\text{CO}_2$ . These results suggest that *Chlorella* JPR-1 has an excellent tolerance to high  $\text{CO}_2$  concentration in the flue gas, and therefore it is recommended as suitable species for  $\text{CO}_2$  biofixation and producing high density biomass.

From Figure 2, the specific growth rate ( $m$ ) of *Chlorella* JPR-1 at each value of  $\text{CO}_2$  content can be obtained and then be depicted in Figure 3, which shows that the specific growth rate of *Chlorella* JPR-1 decreases with

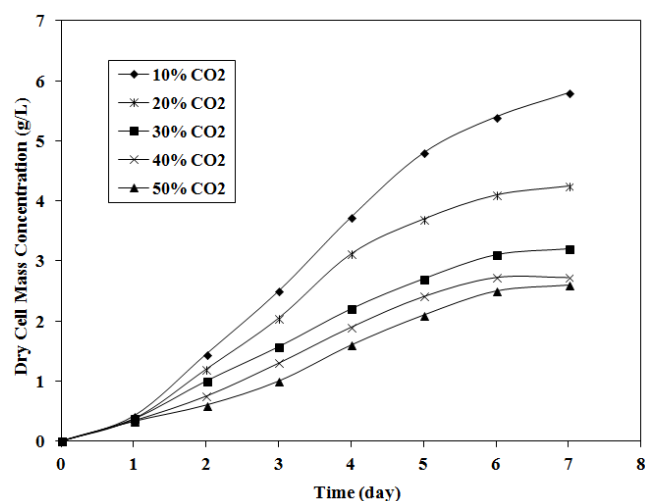


Figure 2. Effect of  $\text{CO}_2$  concentrations on *Chlorella* sp. JPR-1 culture.

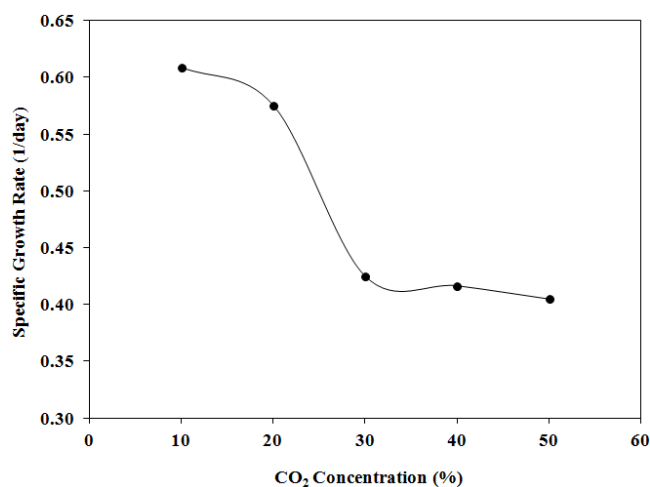


Figure 3. Effect of  $\text{CO}_2$  concentrations on *Chlorella* sp. JPR-1 specific growth rate.

increasing CO<sub>2</sub> concentration in the flue gas feed. The highest specific growth rate was found to be 0.61 1/day when the CO<sub>2</sub> content in the gas feed was 10%. This specific growth rate is almost two times of that of *C. vulgaris* and *C. kessleri* cultured by de Morais and Costa (2007) in a 4 L vertical tubular photobioreactor (VTP) using flue gas containing 6, 12 and 18% CO<sub>2</sub>, which were 0.31 and 0.38 1/day, respectively. However, the specific growth rate found in this work is still lower than that of *Chlorella* JKR-1 cultured with the same CO<sub>2</sub> supply reported by Sung *et al.* (1998), which was 0.67 g/L/day. In addition, this specific growth rate value is also below the specific growth rate of *Chlorella* sp cultured under controlled pH at 5.5 by Devgoswami *et al.* (2011) using CO<sub>2</sub> supply of 4.758 ppm, which was 0.70 g/L/day. The specific growth rate decreased almost linear when the CO<sub>2</sub> concentration in the feed increased from 10 to 30%. A further increase in CO<sub>2</sub> concentration gradually reduces the specific growth rate of *Chlorella* JPR-1.

The carbon contents and carbon fixation rates of *Chlorella* JPR-1 cultured using flue gases with various CO<sub>2</sub> concentrations are tabulated in Table 1. Table 1 shows that the carbon content of the algal cells closely ranged from 0.45 to 0.46 g C/g biomass for five different CO<sub>2</sub> concentrations and indicated that CO<sub>2</sub> concentration does not affect the cell carbon content. Similar results were reported by Zheng *et al.* (2011) who studied the cultivation of *T. subcordiformis* using CO<sub>2</sub> concentration ranged from 1.63-18.37 % and found that the cell carbon contents were between 0.44-0.47 g C/g biomass. In contrast to carbon content, the CO<sub>2</sub> concentration strongly affected the carbon fixation rate. The carbon fixation rate decreased from 1.84 to 0.91 g CO<sub>2</sub>/L.day as the CO<sub>2</sub> concentration in the flue gas increased from 10 to 30%. As expected, further increase in CO<sub>2</sub> concentration was found to gradually reduce the carbon fixation rate due to low specific growth rate. Yun *et al.* (1997) observed that *C. vulgaris* previously adapted to 5% v/v CO<sub>2</sub> and cultivated in wastewater without pH control under 15% v/v CO<sub>2</sub>, performed CO<sub>2</sub> fixation rate of 26.0 g CO<sub>2</sub>/m<sup>3</sup>.h or equal to 0.62 g CO<sub>2</sub>/L.day. Therefore for high efficiency biofixation process, the CO<sub>2</sub> content in the flue gas must be less than 30%, where the microalgae can grow at reasonable speed.

Since CO<sub>2</sub> is the main component in the flue gas, it will almost remain constant during the course of the experiment. In fact, sulfur oxides are also present in the flue gas, mainly as sulfur dioxide (SO<sub>2</sub>). In this experiment, the SO<sub>2</sub> variation was 50-150 ppm, while the concentration of CO<sub>2</sub> gas was kept constant at 20%. The effects of SO<sub>2</sub> concentrations on growth of *Chlorella* JPR-1 are depicted in Figure 4. As SO<sub>2</sub> concentration in the synthetic flue gas increased, the specific growth rate and the maximum cell concentration of *Chlorella* JPR-1 decreased significantly. The specific growth rate of the culture aerated with the synthetic flue gas containing 100 ppm SO<sub>2</sub> was 0.5756 1/day, which is only 38.66% of the control culture. The maximum cell concentration of the culture with 100 ppm SO<sub>2</sub> was 3.15 g/L which is 74.12% of the control culture. Growth of *Chlorella* JPR-1 was totally inhibited with

150 ppm SO<sub>2</sub> where reduction of cells concentration found after three days of cultivation. Without investigating the effect of SO<sub>2</sub> addition at lower concentrations, Westerhoff *et al.* (2010) reported that *Scenedesmus*, *Chlorella* and a mixture of these two cultures died almost immediately upon gaseous addition of 313 ppm SO<sub>2</sub> in 20% CO<sub>2</sub> (balance of gas blend was N<sub>2</sub>), which was simultaneously followed by a drop in pH from 6.2 to 2.6. They also mentioned that since SO<sub>2</sub> is highly soluble in water, it readily partitions from the gas phase and decreases the solution pH.

The carbon content and carbon fixation rate of *Chlorella* JPR-1 cultured using flue gases containing 20% CO<sub>2</sub> and various concentrations of SO<sub>2</sub> are presented in Table 2. It is shown that the carbon content of the algal cells

Table 1. Carbon fixation rate of *Chlorella* sp. JPR-1 culture.

| CO <sub>2</sub> concentration (%) | Carbon Content (g C/g biomass) | CO <sub>2</sub> fixation rate (g CO <sub>2</sub> /L.day) |
|-----------------------------------|--------------------------------|--|
| 10                                | 0.46                           | 1.84   |
| 20                                | 0.46                           | 1.39   |
| 30                                | 0.46                           | 0.91   |
| 40                                | 0.46                           | 0.80   |
| 50                                | 0.45                           | 0.72   |

Table 2. Effect of SO<sub>2</sub> content in flue gas with 20% CO<sub>2</sub> on carbon fixation rate of *Chlorella* sp. JPR-1 culture.

| SO <sub>2</sub> concentration (ppm) | Carbon Content (g C/g biomass) | CO <sub>2</sub> fixation rate (g CO <sub>2</sub> /L.day) |
|-------------------------------------|--------------------------------|--|
| 0                                   | 0.46                           | 1.39   |
| 50                                  | 0.46                           | 0.98   |
| 100                                 | 0.45                           | 0.56   |
| 150                                 | 0.44                           | 0.26   |

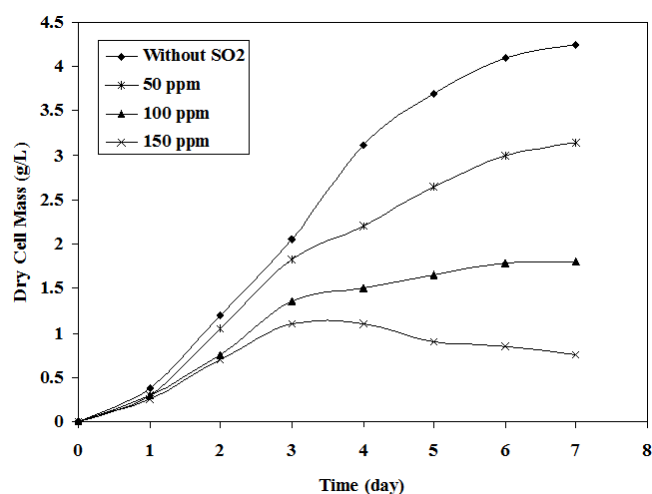


Figure 4. Effect of SO<sub>2</sub> concentrations on *Chlorella* sp. JPR-1 growth.

of four different SO<sub>2</sub> concentrations closely ranged from 0.44 to 0.46 g C/g biomass. The results indicated that SO<sub>2</sub> concentration almost has no effect on the cell carbon content. However, the SO<sub>2</sub> concentration strongly affected the carbon fixation rate. The carbon fixation rate decreased from 1.39 to 0.98 g CO<sub>2</sub>/L.day as the SO<sub>2</sub> concentration in the flue gas increased from 0 to 50 ppm. As expected, further increase in SO<sub>2</sub> concentration was found to sharply reduce the carbon fixation rate to as low as 0.26 g CO<sub>2</sub>/L.day when the SO<sub>2</sub> concentration in the flue gas was 150 ppm due to low specific growth rate.

Considering that growth of most algal strains reported in the literature was completely inhibited, when aerated with CO<sub>2</sub>-air mixture containing SO<sub>2</sub> concentrations higher than 50 ppm (Hauck *et al.*, 1996), *Chlorella* JPR-1 showed a remarkable excellent tolerance to SO<sub>2</sub>. However, the reason for the high tolerance of *Chlorella* JPR-1 to SO<sub>2</sub> is not clear and due to its complexity, it is beyond the scope of this work.

Tolerances of *Chlorella* JPR-1 to NO are shown in Figure 5. When aerated with a gas mixture composed of 20% CO<sub>2</sub>, 5% O<sub>2</sub>, 50 ppm NO, and balance N<sub>2</sub>, the growth of *Chlorella* JPR-1 was only slightly inhibited. The maximum cell concentration and the linear growth rate were almost the same as that obtained in the *Chlorella* JPR-1 cultured by 20% CO<sub>2</sub>-air mixture. However, growth of *Chlorella* JPR-1 was completely retarded when aerated with the 20% CO<sub>2</sub> gas mixture containing 150 ppm NO. Westerhoff *et al.* (2010) cultured *Scenedesmus*, *Chlorella* and a mixture of the two with CO<sub>2</sub> supply from flue gas containing 325 ppm NO and observed a slightly longer lag phase than those cultured without nitrogen oxides, but all grew well and had similar growth rates. The presence of NO may lead to the formation of some nitrite (NO<sub>2</sub><sup>-</sup>) in solution. At concentration of 0-50 mM, nitrite exhibited no inhibitory effect on the growth of algal cultures, but 250 and 500 mM nitrite caused algae to die. Fortunately, NO is only sparingly soluble in water and, thus, very high nitrite concentrations are unlikely to occur.

Table 3 shows the carbon content and carbon fixation rate of *Chlorella* JPR-1 cultured using flue gases containing 20% CO<sub>2</sub> and various concentrations of NO. It is shown that the carbon content of the algal cells of four different NO concentrations were ranged between 0.45-0.46 g C/g biomass. Similar to the CO<sub>2</sub> concentrations, the NO concentrations also do not affect the cell carbon content. Fortunately, the NO concentration only mildly affected the carbon fixation rate. The carbon fixation rate decreased from 1.39 to 0.97 g CO<sub>2</sub>/L.day as the NO concentration in the flue gas increased from 0 to 100 ppm. However, further increase in NO concentration was found to sharply reduce the carbon fixation rate due to low specific growth rate.

Although *Chlorella* JPR-1 showed the limited tolerance to the high concentrations of NO, it could be still applicable for direct CO<sub>2</sub> fixation from LNG flue gas because the flue gas contains low concentrations of NO<sub>x</sub>, less than 100 ppm, and almost no SO<sub>x</sub> (Hauck *et al.*, 1996). Increasing

the inoculating cell concentration was likely to be helpful to enhance the tolerances of *Chlorella* JPR-1 to the toxic compounds.

#### 4. Conclusions

The results of this study show that *Chlorella* JPR-1 exhibited a tolerance to CO<sub>2</sub> content in the flue gas as high as 50%. The *Chlorella* JPR-1 growth was found to be decelerated by the presence of both SO<sub>2</sub> and NO. When *Chlorella* JPR-1 was cultured with the simulated flue gas containing 50 ppm SO<sub>2</sub>, the specific growth rate was 3.15 1/day, which is about 25.88% lower than that of the control culture aerated with the gas mixture containing no toxic compounds, SO<sub>2</sub> and NO. The *Chlorella* JPR-1 could grow even with the synthetic flue gas containing 100 ppm SO<sub>2</sub> and its specific growth rate was 1.8 1/day. A milder effect was observed with a specific growth rate reduction of only 3.53% of the control culture when *Chlorella* JPR-1 was cultured with the simulated gas containing 50 ppm NO. The period for lag phase was slightly increased with increasing of SO<sub>2</sub> and NO concentration resulting in the decrease of the specific growth rate and the maximum cell concentration. These results indicated that *Chlorella* JPR-1 may be applied for

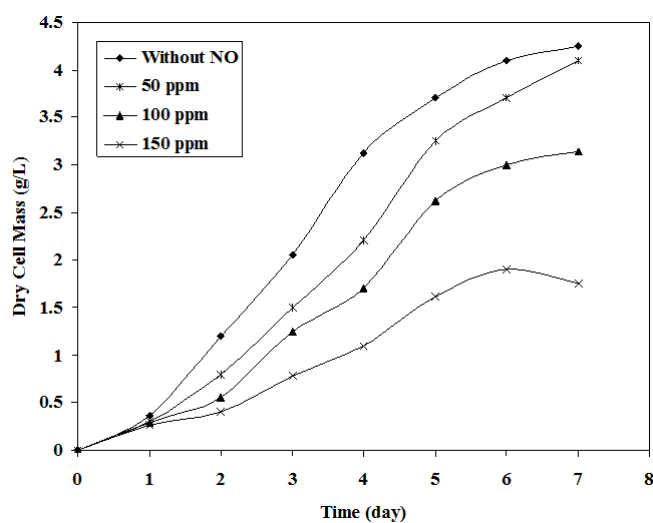


Figure 5. Effect of NO concentrations on *Chlorella* sp. JPR-1 growth.

Table 3. Effect of NO content in flue gas with 20% CO<sub>2</sub> on carbon fixation rate of *Chlorella* sp. JPR-1 culture.

| NO concentration (ppm) | Carbon Content (g C/g biomass) | CO <sub>2</sub> fixation rate (g CO <sub>2</sub> /L.day) |
|------------------------|--------------------------------|--|
| 0                      | 0.46                           | 1.39   |
| 50                     | 0.46                           | 1.23   |
| 100                    | 0.46                           | 0.97   |
| 150                    | 0.45                           | 0.56   |

direct CO<sub>2</sub> fixation from actual flue gas at ambient temperature.

### Acknowledgements

The authors thank the Directorate General of Higher Education, Ministry of National Education the Republic of Indonesia for its financial support through the International Cooperation and International Publication Research Scheme (Hibah Penelitian Kerjasama Luar Negeri dan Publikasi Internasional) 2010 No.: 391.1/H7.5/PL/2010.

### References

- Allard, B. and Templier, J. 2000. Comparison of neutral lipid profile of various trilaminar outer cell wall (TLS)-containing microalgae with emphasis on algaenan occurrence. *Phytochemistry*. 54(4), 369-380.
- de Morais, M. G. and Costa, J.A.V. 2007. Carbon dioxide fixation by *Chlorella kessleri*, *C. Vulgaris*, *Scenedesmus obliquus* and *Spirulina* sp. Cultivated in flasks and vertical tubular photobioreactors. *Biotechnology Letters*. 29, 1349-1352.
- Devgoswami, Ch. R., Kalita, M. C., Talukdar, J., Bora, R. and Sharma, P. 2011. Studies on the growth behavior of *Chlorella*, *Haematococcus* and *Scenedesmus* sp. in culture media with different concentrations of sodium bicarbonate and carbon dioxide gas. *African Journal of Biotechnology*. 10 (61), 13128-13138.
- Dugas, R. and Rochelle, G. 2009. Absorption and desorption rates of carbon dioxide with monoethanolamine and piperazine. *Energy Procedia*. 1 (1), 1163-1169.
- Gavrilescu, M. and Chisti, Y. 2005. Biotechnology – a sustainable alternative for chemical industry. *Biotechnology Advance*. 23, 471-99.
- Gouveia, L. and Oliveira, A. C. 2009. Microalgae as a raw material for biofuels production. *Journal of Industrial Microbiology and Biotechnology*. 36, 269-274.
- Hauck, J. T., Olson, G. J., Scierka, S. J., Perry, M. B. and Ataii, M. M. 1996. Effects of simulated flue gas on growth of microalgae. *Proceedings of 212<sup>th</sup> ACS National Meeting*, Orlando, Florida, USA., August 25-30, 1996.
- Hirata S, Hayashitani M, and Taya M. 1996. Carbon dioxide fixation in batch culture of *Chlorella* sp. using a photobioreactor with a sunlight-collection device. *Journal of Fermentation and Bioengineering*. 18, 470-472.
- Kurano, N., Ikemoto, H., Miyashita, H., Hasegawa, T., Hata, H. and Miyachi, S. 1995. Fixation and utilization of carbon dioxide by microalgal photosynthesis. *Energy Conversion and Management*. 36, 689-692.
- Lee, Y.K. and Shen, H. 2004. Basic culturing techniques. In *Handbook of Microalgal Culture: Biotechnology and Applied Phycology*, A. Richmond, editor. Blackwell Publishing Ltd., Oxford, UK, pp 40-56.
- Malhi, Y., Meir, P. and Brown, S. 2002. Forests, carbon and global climate. *Philosophical Transaction of the Royal Society of London A*. 360, 1567-1591.
- Metzger, P. and Largeau, C. 2005. *Botryococcus braunii*: a rich source for hydrocarbons and related ether lipids. *Applied Microbiology and Biotechnology*. 66, 486-496.
- Silva, H. J., and Pirt, S. J. 1984. Carbon dioxide inhibition of photosynthetic growth of *Chlorella*. *Journal of General Microbiology*. 130, 2833-2838.
- Sung, K. D., Lee, J. S., Shin, C. S. and Park, S. C. 1998. Isolation of a new highly CO<sub>2</sub> tolerant fresh water microalga *Chlorella* KR-1. *Korean Journal of Chemical Engineering*. 15, 449-450.
- Wang, B., Li, Y., Wu, N. and Lan C. Q. 2008. CO<sub>2</sub> bio-mitigation using microalgae. *Applied Microbiology and Biotechnology*. 79, 707-718.
- Westerhoff, P., Hu, Q., Esparza-Soto, M. and Vermaas, W. 2010. Growth parameters of microalgae tolerant to high levels of carbon dioxide in batch and continuous-flow photobioreactors. *Environmental Technology*. 31 (5), 523-532.
- [www.dirgantara-lapan.or.id](http://www.dirgantara-lapan.or.id) [January 25, 2011]
- Yanagi, M., Watanabe, Y. and Saiki, H. 1995. CO<sub>2</sub> fixation by *Chlorella* HA-1 and its utilization. *Energy and Conversion and Management*. 36, 713-716.
- Yoshihara, K., Nagase, H., Eguchi, K., Hirata, K. and Miyamoto, K. 1996. Biological elimination of nitric oxide and carbon dioxide from flue gas by marine microalga NOA-113 cultivated in a long tubular photobioreactor. *Journal of Fermentation and Bioengineering*. 82, 351-354.
- Yun, Y. S., Park, J. M. and Yang, J.W. 1996. Enhancement of CO tolerance of *Chlorella vulgaris* by gradual increase of CO<sub>2</sub> concentration. *Biotechnology Techniques*. 10, 713-716.
- Yun, Y. S., Lee, S. B., Park, J. M., Lee, C. I. and Yang, J. W. 1997. Carbon dioxide fixation by algal cultivation using wastewater nutrients. *Journal of Chemical Technology and Biotechnology*. 69, 451-455.
- Zheng, Y., Chen, Z., Lu, H. B. and Zhang, W. 2011. Optimization of carbon dioxide fixation and starch accumulation by *Tetraselmis subcordiformis* in a rectangular airlift photobioreactor. *African Journal of Biotechnology*. 10 (10), 1888-1901.